Assume all gases are perfect and that the temperature is 298 K unless stated otherwise.

- 2. Suppose that 3.0 mmol of $N_2(g)$ occupies 36 cm³ at 300 K and expands to 60 cm³. Calculate ΔG for the process.
- 3. The change in the Gibbs energy of a certain constant-pressure process was found to fit the expression $\Delta G/J = -85.40 + 36.5(T/K)$. Calculate the value of ΔS for the process.
- 4. When the pressure on a 35-g sample of a liquid was increased isothermally from 1 atm to 3000 atm, the Gibbs energy increased by 12 kJ. Calculate the density of the liquid.
- 5. When 2.00 mol of a gas at 330 K and 3.50 atm is subjected to isothermal compression, its entropy decreases by $25.0 \,\mathrm{J}\,\mathrm{K}^{-1}$. Calculate the final pressure of the gas and ΔG for the compression.
- 6. Calculate the change in chemical potential of a perfect gas that is compressed isothermally from 1.8 atm to 29.5 atm at 40°C.
- 9. Estimate the change in the Gibbs energy of 1.0 L of benzene when the pressure acting on it is increased from 1.0 atm to 100 atm.
- 10. Calculate the change in the molar Gibbs energy of hydrogen gas when it is compressed isothermally from 1.0 atm to 100.0 atm at 298 K.
- 11. The molar Helmholtz energy of a certain gas is given by:

$$A = -\frac{a}{V_{\rm m}} - RT \ln(V_{\rm m} - b) + f(T)$$

where a and b are constants and f(T) is a function of temperature only. Obtain the equation of state of the gas.

Assume all gases are perfect and that the temperature is 298 K unless stated otherwise.

2. Suppose that 3.0 mmol of $N_2(g)$ occupies 36 cm^3 at 300 K and expands to 60 cm^3 . Calculate ΔG for the process.

2. We need G. Start with the definition G = H - TS H = U + pV∴ dG = dU + pdV + Vdp - TdS - SdTNow let us get rid of some terms above. First Law says dU = bq + bWSecond law says $TdS = bq_{rev}$ For a reversible change, $bW = -p_{op}dV$ turns into -pdV∴ dU = TdS - pdVsubstitute into dG to get

$$d\mathbf{G} = Vdp - \mathbf{S}dT$$

Now we are ready: isothermal dT = 0 leads to $d\mathbf{G} = Vdp$ ideal gas V = nRT/p leads to Therefore $\int d\mathbf{G} = \int Vdp = \int nRTdp/p$ isothermal leads to $\int d\mathbf{G} = nRT \ln p_f/p_i$ p_f = nRT/V_f p_i = nRT/V_f divide one eqn. by the other to get $p_f/p_i = V_i/V_f = 36/60$ $\Delta \mathbf{G} = 3 \times 10^{-3} \, \text{mol} \times 8.3144 \, \text{J K}^{-1} \, \text{mol}^{-1}$ $\times 300 \, \text{K} \times \ln 36/60 = -3.8 \, \text{J}$

3. The change in the Gibbs energy of a certain constant-pressure process was found to fit the expression $\Delta G/J = -85.40 + 36.5(T/K)$. Calculate the value of ΔS for the process.

3. We need G and S. Start with definitions G = H - TS H = U + pV∴ dG = dU + pdV + Vdp - TdS - SdTNow let us get rid of some terms above. First Law says dU = dQ + dWSecond law says $TdS = dQ_{rev}$ For a reversible change, $dW = -p_{op}dV$ turns into -pdV∴ dU = TdS - pdVsubstitute into dG to get

$$d\mathbf{G} = Vdp - \mathbf{S}dT$$

We are ready: constant pressure, dp = 0 \therefore d $\mathbf{G} = -\mathbf{S} dT$ $(\partial \mathbf{G}/\partial T)_p = -\mathbf{S}$ $(\partial \mathbf{G}_i/\partial T)_p = -\mathbf{S}_i$ $(\partial \mathbf{G}_i/\partial T)_p = -\mathbf{S}_i$ $\Delta \mathbf{S} = \mathbf{S}_i - \mathbf{S}_i = -\{(\partial \mathbf{G}_i/\partial T)_p - (\partial \mathbf{G}_i/\partial T)_p\}$ $= -(\partial \Delta \mathbf{G}/\partial T)_p$ Given $\Delta \mathbf{G} = -85.40 + 36.5(T/K)$ $(\partial \Delta \mathbf{G}/\partial T)_p = + 36.5 \text{ J K}^{-1}$ $\Delta \mathbf{S} = -36.5 \text{ J K}^{-1}$

4. When the pressure on a 35-g sample of a liquid was increased isothermally from 1 atm to 3000 atm, the Gibbs energy increased by 12 kJ. Calculate the density of the liquid.

4. We need G. Start with definitions G = H - TS H = U + pV∴ dG = dU + pdV + Vdp - TdS - SdTNow let us get rid of some terms above. First Law says dU = dQ + dWSecond law says $TdS = dQ_{rev}$ For a reversible change, dU = dQ + dW∴ dU = TdS - pdVsubstitute into dG to get

$$d\mathbf{G} = Vdp - \mathbf{S}dT$$

Now we are ready: (isothermal) dT = 0 leads to dG = Vdp $\int dG = \int Vdp$ For a liquid V is essentially independent of pressure $\therefore \int dG = V \int dp = V(p_f - p_i)$ $\Delta G = V(3000 - 1) L$ atm $12 \times 10^3 J \times \{0.082056 L$ atm $/ 8.3144 J \}$ = V(3000 - 1). Solve for V, V = .0395Ldensity = m/V = 35/ .0395 L = 886.3 g/L 5. When 2.00 mol of a gas at 330 K and 3.50 atm is subjected to isothermal compression, its entropy decreases by 25.0 J K⁻¹. Calculate the final pressure of the gas and ΔG for the compression.

5. To do this problem, we need to know how S and G change with p.

$$G = H - TS$$
 $H = U + pV$
∴ $dG = dU + pdV + Vdp - TdS - SdT$
Now let us get rid of some terms above.
First Law says $dU = bq + bW$
Second law says $TdS = bq_{rev}$
For a reversible change,
 $bW = -p_{op}dV$ turns into $-pdV$
∴ $dU = TdS - pdV$
substitute into dG to get

 $d\mathbf{G} = Vdp - \mathbf{S}dT$

d**G** is an exact differential, therefore the mixed derivatives are equal:

$$(\partial V/\partial T)_p = -(\partial S/\partial p)_T$$

 $d\mathbf{S} = (1/T)C_p dT - (\partial V/\partial T)_p dp$ general Now we are ready: isothermal dT = 0 leads to $d\mathbf{S} = -(\partial V/\partial T)_p dp$

$$\int_{\mathcal{S}} d\mathbf{S} = \int_{\mathcal{S}} - (\partial V/\partial T)_{p} \, dp$$
ideal gas $pV = nRT$ leads to $V = nRT/p$

$$(\partial V/\partial T)_{p} = nR/p$$

$$\Delta \mathbf{S} = \int_{\mathcal{S}} d\mathbf{S} = \int_{\mathcal{S}} - nR \, dp \, /p = -nR \ln \left(p_{f} \, /p_{i} \right)$$

$$-25 \, \mathrm{J} \, \mathrm{K}^{-1} =$$

$$-2 \, \mathrm{mol} \times 8.3144 \, \mathrm{J} \, \mathrm{K}^{-1} \mathrm{mol}^{-1} \, \ln \left(p_{f} \, /3.5 \right)$$
Solve for p_{f} , $p_{f} = 15.7$ atm
From $d\mathbf{G} = Vdp \cdot \mathbf{S}dT$

$$\int_{\mathcal{S}} d\mathbf{G} = \int_{\mathcal{S}} Vdp \quad \text{when isothermal}$$
and ideal gas eqn $V = nRT/p$ leads to:
$$\Delta \mathbf{G} = \int_{\mathcal{S}} nRTdp \, /p$$
isothermal leads to $\Delta \mathbf{G} = nRT \ln p_{f}/p_{i}$

$$\Delta \mathbf{G} = -\mathrm{T}\Delta \mathbf{S} = -330 \, \mathrm{K} \times \{-25 \, \mathrm{J} \, \mathrm{K}^{-1} \}$$

$$= +8.25 \, \mathrm{kJ}$$
Note
$$\Delta \mathbf{G}_{T} = \Delta \mathbf{H} \cdot \mathrm{T}\Delta \mathbf{S}$$
ideal gas $(\partial \mathbf{H}/\partial \mathbf{P})_{T} = 0$ and $dT = 0$ gives

ideal gas $(\partial H/\partial p)_T = 0$, and dT = 0 gives $\Delta H = 0$ also leads to $\Delta G_T = -T\Delta S$ for this problem.

6. Calculate the change in chemical potential of a perfect gas that is compressed isothermally from 1.8 atm to 29.5 atm at 40°C.

6. Chemical potential is Gibbs energy per mole, so we need **G**:

$$G \equiv H - TS$$
 $H \equiv U + pV$
∴ $dG = dU + pdV + Vdp - TdS - SdT$
First Law says $dU = \delta q + \delta W$
Second law says $TdS = \delta q_{rev}$
For a reversible change,
 $\delta W = -p_{op}dV$ turns into $-pdV$
∴ $dU = TdS - pdV$
substitute into dG to get

 $d\mathbf{G} = Vdp - \mathbf{S}dT$

isothermal, at
$$T$$
, $\int d\mathbf{G} = \int V dp$
 $\mathbf{G}_f(T) = \mathbf{G}_i(T) + \int_{p1}^{p2} V dp$.

For an ideal gas

$$\mathbf{G}_{f}(T) = \mathbf{G}_{i}(T) + \int_{1}^{p} \frac{nRT}{p} dp.$$

Define the free energy per mole (the chemical potential, μ):

$$\mu_f(T) = \mu_i(T) + RT \ln \frac{p_2}{p_1}$$
 (ideal gas)

$$\Delta\mu(T) = +RT \ln \frac{p_2}{p_1}$$

=
$$8.3144 \text{ J K}^{-1} \text{mol}^{-1} \times 313 \text{ K} \times \ln(29.5/1.8)$$

= $+7.3 \text{ kJ mol}^{-1}$

9. Estimate the change in the Gibbs energy of 1.0 L of benzene when the pressure acting on it is increased from 1.0 atm to 100 atm.

9. We need G. Start with definition G = H - TS H = U + pV

:. $d\mathbf{G} = d\mathbf{U} + pdV + Vdp - Td\mathbf{S} - \mathbf{S}dT$ Now let us get rid of some terms above. First Law says $d\mathbf{U} = \delta q + \delta W$

Second law says $TdS = \delta q_{rev}$

For a reversible change,

 $\delta W = -p_{op} dV \qquad \text{turns into } -p dV$

 $\therefore dU = TdS - pdV$

substitute into dG to get

$$d\mathbf{G} = Vdp - \mathbf{S}dT$$

Now we are ready: dT=0 (isothermal), at T, $\int d\mathbf{G} = \int V dp$

$$\Delta G(T) = \int_{p_1}^{p_2} V dp = V(p_2 - p_1)$$

= 1 L(100-1) atm = 99 L atm

= 99 L atm \times {8.3144 J /0.082056 L atm }

= 10 kJ

10. Calculate the change in the molar Gibbs energy of hydrogen gas when it is compressed isothermally from 1.0 atm to 100.0 atm at 298 K.

10. We need G. Start with definition $G \equiv H - TS$ $H \equiv U + pV$

∴ dG = dU + pdV + Vdp - TdS - SdTNow let us get rid of some terms above. First Law says dU = bq + bWSecond law says $TdS = bq_{rev}$ For a reversible change, $bW = -p_{op}dV$ turns into -pdV∴ dU = TdS - pdV

substitute into dG to get

 $d\mathbf{G} = Vdp - \mathbf{S}dT$

 $\int d\mathbf{G} = \int V dp$ when isothermal (dT = 0) and ideal gas V = nRT/p leads to: $\Delta \mathbf{G} = \int nRT dp/p$ isothermal leads to $\Delta \mathbf{G} = nRT \ln p_f/p_i$ $\Delta \mathbf{G} = 1 \mod \times 8.3144 \text{ J K}^{-1} \mod^{-1} \times 298 \text{ K}$ $\times \ln(100/1) = + 11 \text{ kJ mol}^{-1}$ 11. The molar Helmholtz energy of a certain gas is given by:

given by.
$$A = -\frac{a}{V_{\rm m}} - RT \ln(V_{\rm m} - b) + f(T)$$

where a and b are constants and f(T) is a function of temperature only. Obtain the equation of state of the gas. 11. We need A. Start with definition

$$A \equiv U - TS$$
 $dA = dU - TdS - SdT$

Now let us get rid of some terms above.

First Law says
$$dU = \delta q + \delta W$$

Second law says
$$TdS = \delta q_{rev}$$

For a reversible change,

$$\mathfrak{d}W = -p_{op}dV \qquad \text{turns into } -pdV$$

$$dU = TdS - pdV$$

substitute into dA to get

$$d\mathbf{A} = - p dV - \mathbf{S} dT$$

What we need is an expression for p

$$(\partial A/\partial V)_T = -p$$

This allows us to take from

$$A = -\frac{a}{V_{\rm m}} - RT \ln(V_{\rm m} - b) + f(T)$$

the derivative of the expression with respect to V:

$$-p = (\partial A/\partial V)_T = a/V^2 - RT \{1/(V-b)\}$$

$$p = -a/V^2 + RT \{1/(V-b)\}$$

is the equation of state.

2. Calculate the equilibrium pressure for the conversion of graphite to diamond at 25°C. The densities of graphite and diamond may be taken to be 2.55 and 3.51 g cm⁻³, respectively, independent of pressure.

 $\Delta_{f} H^{\ominus}$ (diamond) = 0.4532 kcal mol⁻¹ S^{\ominus} (298 K) = 0.5829 cal K⁻¹ mol⁻¹ for diamond = 1.3609 cal K⁻¹ mol⁻¹ for graphite

5. Recognizing that the Gibbs free energy of fusion of ice at 0°C and 1 atm is equal to zero, and assuming the heat capacities of ice and supercooled water to be constant, derive by integration of the Gibbs-Helmholtz equation an expression for the Gibbs free energy of fusion of ice as a function of temperature. Also derive expressions for $\Delta_{fus} \mathbf{H}$ and $\Delta_{fus} \mathbf{S}$ as functions of temperature. If the specific heat of fusion of ice at 0°C and 1 atm is 79.7 cal g⁻¹ and the specific heat capacities of ice and water are 0.48 and 1.00 cal K⁻¹ g⁻¹ respectively, what are the molar values for $\Delta_{fus} \mathbf{G}$, $\Delta_{fus} \mathbf{H}$, and $\Delta_{fus} \mathbf{S}$ at -3°C?

EXAMPLE: 2. Calculate the equilibrium pressure for the conversion of graphite to diamond at 25°C. The densities of graphite and diamond may be taken to be 2.55 and 3.51 g cm⁻³, respectively, independent of pressure.

 $\Delta_t \mathbf{H}^{\ominus}$ (diamond) = 0.4532 kcal mol⁻¹

	S [⊕] (298 K)			
	cal K ⁻¹ mol ⁻¹			
diamond	0.5829			
graphite	1.3609			

Question:

graphite(298 K, p) \rightarrow diamond(298 K, p) Find p at equilibrium.

Solution:

graphite(298, 1)
$$\rightarrow$$
 diamond(298, 1) (a) graphite(298, 1) \rightarrow graphite(298, p) (b) diamond(298, 1) \rightarrow diamond(298, p) (c) (a) -(b) +(c) =

graphite(298 K, p) \rightarrow diamond(298 K, p)

Given for step (a): graphite \rightarrow diamond $\Delta_t H^{\ominus} = 0.4532$ (298 K, 1 bar) (298, 1 bar) kcal mol⁻¹ $G \equiv H - TS$ At constant T = 298 K, dT = 0, $\therefore \Delta G_T = \Delta H - T \Delta S$ and $\Lambda \mathbf{G}^{\ominus} = \Lambda \mathbf{H}^{\ominus} - T \Lambda \mathbf{S}^{\ominus}$ $\Delta G_a^{\odot} = 453.2 \text{ cal}$ -298 K (0.5829 -1.3609) cal K⁻¹ mol⁻¹ = 685 calFor (b) and (c): As already derived in previous example,

$$d\mathbf{G} = Vdp - \mathbf{S}dT \qquad dT = 0$$

 $\int d\mathbf{G} = \int V dp = V \int dp$ since densities are given as independent of pressure.

$$\Delta G_b = (12/2.55) \times 10^{-3} \text{ L } [p-1]$$

$$\Delta G_c = (12/3.51) \times 10^{-3} L [p-1]$$

Since *p* is the pressure at which the two phases are at equilibrium, $\Delta G(p) = 0$.

$$0 = \Delta \mathbf{G}_a - \Delta \mathbf{G}_b + \Delta \mathbf{G}_c$$

0= 685+{-(12/2.55)+(12/3.51)}×10⁻³(
$$p$$
-1)
×(1.987 cal)/(8.3144×10⁻² L bar)
Solve for p
 p = 22269 bar

EXAMPLE:

5. Recognizing that the Gibbs free energy of fusion of ice at 0°C and 1 atm is equal to zero, and assuming the heat capacities of ice and supercooled water to be constant, derive by integration of the Gibbs-Helmholtz equation an expression for the Gibbs free energy of fusion of ice as a function of temperature. Also derive expressions for $\Delta_{fus} \mathbf{H}$ and $\Delta_{fus} \mathbf{S}$ as functions of temperature. If the specific heat of fusion of ice at 0°C and 1 atm is 79.7 cal g⁻¹ and the specific heat capacities of ice and water are 0.48 and $1.00 \text{ cal K}^{-1} \text{ g}^{-1}$ respectively, what are the molar values for $\Delta_{fus}G$, $\Delta_{fus}H$, and $\Delta_{fus}S$ at -3°C?

Question:

ice (1 atm,
$$T$$
) \rightarrow liquid (1 atm, T) \rightarrow ind: $\Delta_{fus}\mathbf{G}$ $\Delta_{fus}\mathbf{H}$ $\Delta_{fus}\mathbf{S}$ as a function of T

Consider the steps:

ice (1 atm, 273.2 K)
$$\rightarrow$$
 liquid (1 atm, 273.2 K) (a) ice (1 atm, 273.2 K) \rightarrow ice (1 atm, T) (b) liq (1 atm, 273.2 K) \rightarrow liq (1 atm, T) (c) $\Delta_{fus}G_T = \Delta G_a - \Delta G_b + \Delta G_c$
 $G = H - TS$

$$\Delta G_a = 0 \qquad \text{ice and liq are at equilibrium}$$

$$\Delta G_b = \Delta H_b - (TS_{ice,T} - 273.2 S_{ice,273})$$

$$\Delta G_c = \Delta H_c - (TS_{liq,T} - 273.2 S_{liq,273})$$

$$\Delta H_b = \int_{273}^{T} C_p^{ice} dT = 0.48 \times 18 (T-273)$$

$$\Delta H_c = \int_{273}^{T} C_p^{L/Q} dT = 1.0 \times 18 (T-273)$$

$$S_{ice,T} = S_{ice,273} + \int_{273}^{T} (C_p^{ice}/T) dT$$

$$= S_{ice,273} + 0.48 \times 18 \ln(T/273)$$

$$S_{liq,T} = S_{liq,273} + \int_{273}^{T} (C_p^{liq}/T) dT$$

$$= S_{liq,273} + 1.0 \times 18 \ln(T/273)$$

$$\Delta \mathbf{G}_{b} = 0.48 \times 18 \ (T-273)$$

$$- T[\mathbf{S}_{ice,273} + 0.48 \times 18 \ ln(T/273)] + 273 \ \mathbf{S}_{ice,273}$$

$$= 0.48 \times 18 \ (T-273) - (T-273) \mathbf{S}_{ice,273}$$

$$\Delta \mathbf{G}_{c} = 1.0 \times 18 \ (T-273)$$

$$- T[\mathbf{S}_{liq,273} + 1.0 \times 18 \ ln(T/273)] + 273 \ \mathbf{S}_{liq,273}$$

$$= 1.0 \times 18 \ (T-273) - (T-273) \mathbf{S}_{liq,273}$$

$$\Delta_{fus} \mathbf{G}_{T} = \Delta \mathbf{G}_{a} - \Delta \mathbf{G}_{b} + \Delta \mathbf{G}_{c}$$

$$= 0 - 0.48 \times 18 \ (T-273) + (T-273) \mathbf{S}_{liq,273}$$

$$+ 1.0 \times 18 \ (T-273) - (T-273) \mathbf{S}_{liq,273}$$

$$= (1.0 - 0.48) \times 18[(T-273) - T \ ln(T/273)]$$

$$+ (T-273)(\mathbf{S}_{ice,273} - \mathbf{S}_{liq,273})$$

$$(\mathbf{S}_{ice,273} - \mathbf{S}_{liq,273}) = -\Delta_{fus} \mathbf{H}_{273} \ /273 = -79.7 \times 18/273$$

$$\therefore \Delta_{fus} \mathbf{G}_{T} = 18 \times \{ (T-273)[(1.0 - 0.48) - 79.7/273]$$

-
$$(1.0-0.48)T \ln(T/273)$$
}
$$\Delta_{fus}G_T = -1120.7 + 56.61T - 9.36T \ln T \text{ cal } A_{nswer}$$

$$\Delta_{fus} \mathbf{H}_{T} = \Delta \mathbf{H}_{a} - \Delta \mathbf{H}_{b} + \Delta \mathbf{H}_{c}$$

$$= 79.7 \times 18 - 0.48 \times 18 \ (T-273)$$

$$+1.0 \times 18 \ (T-273)$$

$$\Delta_{fus} \mathbf{H}_{T} = \{ \ (T-273)(1.0-0.48) + 79.7 \} \times 18$$

$$\Delta_{fus} \mathbf{H}_{T} = -1120.7 + 9.36T \ \text{cal } \Delta_{nswer}$$

$$\Delta_{fus}\mathbf{S}_{T} = \Delta\mathbf{S}_{a} - \Delta\mathbf{S}_{b} + \Delta\mathbf{S}_{c}$$
 $d\mathbf{S} = \delta q_{REV}/T$
 $\Delta\mathbf{S}_{a} = 79.7 \times 18/273$
 $d\mathbf{S} = (\partial \mathbf{S}/\partial T)_{p}dT + (\partial \mathbf{S}/\partial p)_{T}dp$
 $d\mathbf{S} = (C_{p}/T)dT \text{ since } dp = 0$
 $\Delta\mathbf{S}_{b} = \int_{273}^{T} C_{p}^{ice}dT/T = 0.48 \times 18 \ln(T/273)$
 $\Delta\mathbf{S}_{c} = \int_{273}^{T} C_{p}^{L/Q}dT/T = 1.0 \times 18 \ln(T/273)$
 $\Delta_{fus}\mathbf{S}_{T} = \Delta\mathbf{S}_{a} - \Delta\mathbf{S}_{b} + \Delta\mathbf{S}_{c}$
 $\Delta_{fus}\mathbf{S}_{T} = 79.7 \times 18/273 - 0.48 \times 18 \ln(T/273)$
 $+ 1.0 \times 18 \ln(T/273)$
 $\Delta_{fus}\mathbf{S}_{T} = \{(1.0 - 0.48)\ln(T/273) + 79.7/273\} \times 18$
 $\Delta_{fus}\mathbf{S}_{T} = -47.25 + 9.36\ln T \text{ cal}$
 $\Delta_{fus}\mathbf{S}_{T} = -47.25 + 9.36\ln T \text{ cal}$
 $\Delta_{fus}\mathbf{S}_{T} = -47.25 + 9.36\ln T \text{ cal}$
get
 $\Delta_{fus}\mathbf{G}_{T} = -1120.7 + 9.36T \text{ cal}$
 $\Delta_{fus}\mathbf{G}_{T} = -1120.7 + 56.61T - 9.36T \ln T \text{ cal}$
yes, agrees with $\Delta_{fus}\mathbf{G}_{T}$ obtained from sum of a,b,c.
 $\Delta_{fus}\mathbf{G}_{T}/T = -1120.7/T + 56.61 - 9.36 \ln T$
Now take the derivative
 $[\partial(\Delta\mathbf{G}/T)/\partial T]_{p} = +1120.7/T^{2} - 9.36/T$
This indeed agrees with
 $-\Delta_{fus}\mathbf{H}/T^{2} = +1120.7/T^{2} - 9.36/T$

The problem suggested integrating the Gibbs Helmholtz eq. as a strategy:

 $[\partial (\mathbf{G}_t/T)/\partial T]_p = -\mathbf{H}_t/T^2$ applied to liquid (1atm, T) $[\partial (\mathbf{G}_i/T)/\partial T]_p = -\mathbf{H}_i/T^2$ applied to ice (1atm, T) $[\partial (\Delta \mathbf{G}/T)/\partial T]_p = -\Delta \mathbf{H}/T^2$

So if we had started out with

 $[\partial(\Delta \boldsymbol{G}/T)/\partial T]_p = -\Delta \boldsymbol{H}/T^2$ and integrated, $\int d(\Delta \boldsymbol{G}/T) = \int (-\Delta \boldsymbol{H}/T^2)dT$

This would mean that we need only to calculate $\Delta_{fus} H_T = -1120.7 + 9.36T$ cal

just as we did using steps a,b,c above.

we would have obtained

$$\int d(\Delta G/T) = \int (+1120.7/T^2 - 9.36/T)dT$$

$$(\Delta G/T) = -1120.7/T - 9.36 \ln T + constant$$

Let us now compare this with the $\Delta_{fus} G_T/T$ that we had calculated using the steps a,b,c above: $\Delta_{fus} G_T/T = -1120.7/T + 56.61 - 9.36 \ln T$

It checks! and we find the constant of integration is +56.61 cal K⁻¹

at -3°C (270 K) event is spontaneous in reverse: $\Delta_{fus} G_T = -1120.7 + 56.61 T - 9.36 T \ln T = +15.67$ cal mol⁻¹ $\Delta_{fus} H_T = -1120.7 + 9.36 T = +1406.5$ cal mol⁻¹ $\Delta_{fus} S_T = -47.25 + 9.36 \ln T = +5.151$ cal mol⁻¹ K⁻¹



4. Suppose 2.000 mol of neon (assumed to be an ideal gas) is confined in a strong to the strong stro	mg,
rigid container of volume 50.0 L at 304.66 K. The system is heated until 5000.	J of
heat has been added.	

For this process, draw your initial a	and final _J	pictures here	
$n_{initial} = V_{initial} = T_{initial} = p_{initial} = p_{initial}$	\rightarrow	$n_{final} = V_{final} = T_{final} = p_{final} = 0$	***************************************
(a) The molar heat capacity of the a is the molar heat capacity of mular beat capacity of mular bear bear bear bear bear bear bear be	neon gas?	□equation:	
	***************************************		mol ⁻¹
(b) Calculate the original pres			
Using: □given in the problem □defir	nition:	□equation:	
		p _{initial} =	atm
(c) Determine q for the system	during th	ne heating process	
Using: □given in the problem □defir	nition:	□equation:	
		q =	J

Using: □given in the problem □definition:	□equation:	
	w =	J
(e) Compute the temperature of the gas container itself has zero heat capacity)	after the heating. (Assume	that the
Jsing: □given in the problem □definition:	□equation:	
	$\mathcal{T}_{\mathit{final}}$ =	K
Jsing: □given in the problem □definition:	□equation:	
	p _{final} =	atm
· ··		at m
process.		
process.	rgy of the gas during the he	
process.	rgy of the gas during the he	
(g) Compute change in the internal ene pprocess. Using: □given in the problem □definition:	rgy of the gas during the he	

Problem 4. continued on this page. (h) Compute the change in enthalpy of the	ne gas during the heating pro	ocess.
Using: □given in the problem □definition:	□equation:	
	∆ H =	J
(i) Correct answer to part (h) exceeds the amount why this is not a violation of the law of conse		xplain
Using: □given in the problem □definition:	☐equation:	
(j) Show the type of process when change of Using: □given in the problem □definition:	enthalpy equals the heat abso □equation:	orbed
(k) <i>Calculate the change in entropy</i> for the Using: □given in the problem □definition:	nis constant volume heating. □equation:	
	·	
	∆ S =	J K ⁻¹

Problem 4. continued on this page (1) Using the definition of **G** in terms of **H** and **S**, what is the expression for the change in Gibbs free energy? Using: □given in the problem □definition: Dequation: (m) Calculate the change in Gibbs free energy for this constant volume heating. The standard entropy value for neon gas is S° at 298.15 K = 146.22 J K⁻¹ mol⁻¹ Using: □given in the problem □definition: □equation: $\Lambda G =$ (n) Suppose we had taken the neon gas from the original initial state to the same final state through a different path [for example, the 2-step sequence of : (i) isothermal compression to the final pressure, followed by (ii) constant pressure expansion to the final volume] instead, which of the following quantities for the overall 2-step process will be the same as calculated above for the constant volume heating? Circle as many as apply: ΔT ΔV w ΔE ΔH ΔS ΔG Δp Δn q

4. Suppose 2.000 mol of neon (assumed to be an <u>ideal gas</u>) is confined in a strong, rigid container of volume 50.0 L at 304.66 K. The system is heated until 5000 J of heat has been added.

For this process, draw your initial and final pictures here $\begin{bmatrix}
n_{initial} = 2.000 \text{ mol} \\
V_{initial} = 50.0 \text{ L} \\
T_{initial} = 304.66 \text{ K} \\
p_{initial} = ? \text{ atm}
\end{bmatrix}$ $q = \begin{cases}
q = \\
+5000 \text{ J} \\
T_{final} = ? \text{ K} \\
T_{final} = ? \text{ atm}
\end{cases}$

(a) The molar heat capacity of the gas does not change during the heating. What is the molar heat capacity of neon gas?

Using: \square given in the problem \square definition: ideal gas \square equation: $\frac{1}{2}$ m $\langle u^2 \rangle = (3/2)k_BT$ for one mole of a monatomic ideal gas, $E = E_0 + \frac{1}{2}$ m $\langle u^2 \rangle N_{\text{Avog}} = E_0 + (3/2)RT$ so that $C_V = (3/2)R = (3/2)(8.31451 \text{J K}^{-1} \text{ mol}^{-1}) = 12.472 \text{J mol}^{-1}$

(b) Calculate the original pressure inside the vessel (in atm)

Using: \square given in the problem \square definition: \square equation: pV=nRT p (50.0 L) =(2.0 mol)(0.0820578 L atm K⁻¹ mol⁻¹)(304.66 K) p = 1.00 atm $p_{initial} = 1.00 \text{ atm}$

(c) **Determine** q for the system during the heating process

Using: ☑given in the problem ☐definition: ☐equation: q = +5000 J

(d)	Determine	w for the	system	during the	heating process
-----	-----------	-----------	--------	------------	-----------------

Using: \square given in the problem \square definition: $dw = -p_{oppposing}dV$ \square equation: dV = 0 (rigid container no change in V) therefore dw = 0 w = 0 \square

(e) **Compute the temperature of the gas** after the heating. (Assume that the container itself has zero heat capacity)

Using: \square given in the problem \square definition: $d\mathbf{q} = CdT$ \square equation: C = (3/2)R does not change (given) so $\mathbf{q} = C\Delta T = C(T_{final} - T_{initial})$ 5000 J = 2.0 mol (3/2)(8.31451J K⁻¹ mol⁻¹)(T_{final} - 304.66 K) Solve for T_{final}

(f) **Compute the pressure** (in atm) inside the vessel after the heating.

Using: \square given in the problem \square definition: \square equation: pV = nRT p_{final} (50.0 L) =(2.0 mol)(0.0820578 L atm K⁻¹ mol⁻¹)(505.11 K) Solve for p_{final} = 2.0×0.0820578×505.11 / 50.0

 $p_{final} = 1.658$ atm

(g) Compute change in the internal energy of the gas during the heating process.

Using: □given in the problem □definition:

 \blacksquare equation: $\Delta E = q + w$

First law provides $\Delta E = q + w = 5000 + 0$

 $\Delta E = 5000$

Problem 4. continued c	on this	page.
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(h) Compute the change in enthalpy of the gas during the heating process.

Using: \square given in the problem \square definition: H = E + pV \square equation:

H = E + pV means that the change is

 $\Delta H = \Delta E + p_{final} V_{final} - p_{initial} V_{initial}$

= 5000 J + (1.658 atm - 1.000 atm)50.0 L

 $\times (8.31451 \text{ J K}^{-1} \text{ mol}^{-1})/(0.0820578 \text{ L atm K}^{-1} \text{ mol}^{-1}) = 5000+3333.6$

 $\Delta H = 8333.6$

(i) Correct answer to part (h) exceeds the amount of heat actually added. *Explain* **why** this is not a violation of the law of conservation of energy.

Using: □given in the problem ☑definition: First law: *E* is conserved □equation: The law of conservation of energy applies to energy, not enthalpy.

(j) **Show** the type of process when change of enthalpy equals the heat absorbed

Using: \square given in the problem \square definition: H = E + pV, $\triangle E = q + w \square$ equation:

Constant pressure process: $w_p = -p_{opposing}(V_{final} - V_{initial})$

and $\Delta \mathbf{H} = \Delta \mathbf{E} + p(V_{final} - V_{initial})$

Combining this with First Law: $\Delta E = q_p + w_p$

leads to $\Delta H = q_p$

(k) Calculate the change in entropy for this constant volume heating.

Using: \square given in the problem \square definition: $dS = dq_{rev}/T$ \square equation:

Carry out the heating at constant volume in a reversible manner, $dq = C_V dT = dq_{rev}$, so that $dS = C_V dT/T$, which when summed up gives

 $\Delta S = C_V \ln(T_{final}/T_{initial}) = 2.0 \text{ mol} \times 3/2 \times (8.31451 \text{J K}^{-1} \text{mol}^{-1}) \ln(505.11/304.66)$

J K⁻¹ Λ **S** = 12.61

Problem 4. continued on this page

(l) Using the definition of **G** in terms of **H** and **S**, what is the expression for the change in Gibbs free energy?

```
Using: \squaregiven in the problem \squaredefinition: \mathbf{G} \equiv \mathbf{H} - T\mathbf{S} \squareequation: \Delta \mathbf{G} = \Delta \mathbf{H} - (T_{final} \mathbf{S}_{final} - T_{initial} \mathbf{S}_{initial})
```

(m) Calculate the change in Gibbs free energy for this constant volume heating. The standard entropy value for neon gas S° at 298.15 K = 146.22 J K⁻¹ mol⁻¹.

```
Using: \blacksquaregiven in the problem \mathbf{S}^{\circ}_{298.15 \text{ K}} = 146.22 \text{ J K}^{-1} \text{ mol}^{-1} \blacksquare definition: \mathbf{S}_{0\text{K}} = 0
                                  \blacksquare equation: \Delta S_V = C_V \ln(T_{final}/T_{initial}) derived in part (k)
From \mathbf{q}_{rev}/T = -\mathbf{w}_{rev}/T when \Delta \mathbf{E} = 0, we find \Delta \mathbf{S}_T = nR \ln(V_{final}/V_{initial})
Third law plus equation derived in part (k) and above gives
S_{final} = S_{298 \text{ K}}^{\circ} + C_V \ln(T_{final}/298.15) + \Delta S (1 \text{ atm} \rightarrow 1.658 \text{ atm})
        = 146.22 + 2.0(3/2)(8.31451) \ln (505.11/298.15)
                                                                          + 2.0(8.31451)ln (1/1.658)
        = 146.22 + 13.15 - 8.41 = 150.96 \text{ J K}^{-1}
S_{initial} = S_{298 \text{ K}}^{\circ} + C_V \ln(T_{initial} / 298.15)
                                                             at 1 atm
        = 146.22 + 2.0(3/2)(8.31451) \ln (304.66/298.15)
        = 146.22 + 0.539 = 146.76 \text{ J K}^{-1}
  \Delta G = \Delta H - (T_{final} S_{final} - T_{initial} S_{initial})
        = 8333.6 J - (505.11×150.96 - 304.66×146.76) J
        = 8333.6 - 31 539.5 = -23 205.9 J
                                                                                        \Delta G = -23\ 205.9\ J
```

(n) Suppose we had taken the neon gas from the original initial state to the same final state through a different path [for example, the 2-step sequence of: (i) isothermal compression to the final pressure, followed by (ii) constant pressure expansion to the final volume] instead, which of the following quantities for the overall 2-step process will be the same as calculated above for the constant volume heating? **Circle as many as apply:**

_										
	(∆7)	(∆p)	(\(\Lambda \(V \)	(∆n)	q	w	(∆ <i>E</i>)	(∆ <i>H</i>)	(∆S)	(∆G)

 $C_p = 28.3144 \text{ J K}^{-1} \text{ mol}^{-1}$

Example:

Two moles of a gas whose equation of state is $\rho V = RT + a\rho$ where a has the following values

00 S	T, K	300	400	500
	a, L mol ⁻¹	0.020	0.025	0.030

undergoes isothermal compression at 300 K from 1 atm to 11 atm.

Questions:

Calculate $\Delta \mathbf{G}$, $\Delta \mathbf{S}$, $\Delta \mathbf{H}$ for the gas.

EXAMPLE:

B. All changes in B are isothermal, that is added to section A and the piston moves section A. Calculate for the gas in each adiabatic piston into two sections ${\mathcal A}$ and 3. Consider a perfect gas contained in a temperature constant. There is 2.00 mol cylinder and separated by a frictionless of the gas in each section. Initially $T_A =$ Calculate ΔS of the total system and its $T_{\mathcal{B}} = 300 \text{ K}, V_{\mathcal{A}} = V_{\mathcal{B}} = 2.00 \text{ L}.$ Heat is Calculate the work done by the gas in a thermostat surrounds ${\cal B}$ to keep its to the right reversibly until the final section: ΔU , q, ΔS , ΔA , ΔH , ΔG . volume of section $\mathcal B$ is 1.00 L . surroundings. Assume $C_V = 20 \text{ J K}^{-1} \text{ mol}^{-1}$

Example:

Two moles of a gas whose equation of state is pV = RT + ap where a has the following values

a, L mol ⁻¹	<i>T</i> , K
0.020	300
0.025	400
0.030	500

undergoes isothermal compression at 300 K from 1 atm to 11 atm.

Questions:

Calculate ΔG , ΔS , ΔH for the gas.

$$pV = RT + a(T)p$$

300 K 1 atm 2 mol

$$\rightarrow$$
 d $T = 0$

 V_f 300 K $\frac{1}{dT} = 0$ 11 atm 2 mol

From G = H - TS and H = U + pV $d\mathbf{G} = d\mathbf{H} - Td\mathbf{S} - \mathbf{S}dT$ = dU + pdV + Vdp - TdS - SdTapply $dS = dq_{REV}/T$ and $dU = dq_{REV} + dW_{REV} = dq_{REV} - pdV$ to derive $d\mathbf{G} = -\mathbf{S}dT + Vdp$ For this problem, dT = 0 leads to

$$\Delta \mathbf{G} = n \int_{-\infty}^{11} (\frac{RT}{p} + a) dp$$

 $\Delta G = 2\{0.08205 \times 300 \times \ln(11/1) + 100 \times \ln(11/1)\}$ $0.020 \times (11-1) \times (1.987/0.08205)$ cal

Consider the state function
$$S(T,p)$$
:

$$dS = (\partial S/\partial T)_{p}dT + (\partial S/\partial p)_{T}dp$$

First derive $(\partial S/\partial p)_T$:

dG = -SdT + Vdp derived above leads to equal cross-derivatives

$$-(\partial S/\partial p)_T = (\partial V/\partial T)_p$$

From the eqn of state:

pV = RT + a(T)p we rearrange to get

$$V = (RT/p) + a(T)$$

$$(\partial V/\partial T)_p = (R/p) + da/dT$$

=
$$(R/p) + 0.5 \times 10^{-4}$$
 given table

To get ΔS when dT = 0,

$$\Delta S = -n \int_{-\infty}^{11} (\frac{R}{p} + 0.5 \times 10^{-4}) dp$$

$$\Delta S = -2\{0.08205 \times \ln(11/1) + 0.5 \times 10^{-4} \times (11-1)\} \times (1.987/0.08205)$$
cal K⁻¹

Consider the state function
$$\mathbf{H}(T,p)$$
: $d\mathbf{H} = (\partial \mathbf{H}/\partial T)_p dT + (\partial \mathbf{H}/\partial p)_T dp$ First derive $(\partial \mathbf{H}/\partial p)_T$: using cross-derivatives (see lectures) $-(\partial \mathbf{H}/\partial p)_T = -T(\partial V/\partial T)_p + V$ From the eqn of state: $pV = RT + a(T)p$ we rearrange to get $V = (RT/p) + a(T)$ $(\partial V/\partial T)_p = (R/p) + da/dT$ $= (R/p) + 0.5 \times 10^{-4}$ $-(\partial \mathbf{H}/\partial p)_T = -T(\partial V/\partial T)_p + V$ $= -(RT/p) -0.5 \times 10^{-4}T + (RT/p) + a$ $= -0.5 \times 10^{-4}T + a = 0.035$ at $T = 300$ K To get $\Delta \mathbf{H}$ when $dT = 0$, $\Delta \mathbf{H} = -n \int_{-1}^{1} 0.035 dp$

$$\Delta H = -2 \times 0.035 \times (11-1) \times 1.987 / 0.08205$$

EXAMPLE:

3. Consider a perfect gas contained in a cylinder and separated by a frictionless adiabatic piston into two sections \mathcal{A} and \mathcal{B} . All changes in \mathcal{B} are isothermal, that is a thermostat surrounds \mathcal{B} to keep its temperature constant. There is 2.00 mol of the gas in each section. Initially $T_{\mathcal{A}} = T_{\mathcal{B}} = 300 \text{ K}$, $V_{\mathcal{A}} = V_{\mathcal{B}} = 2.00 \text{ L}$. Heat is added to section \mathcal{A} and the piston moves to the right reversibly until the final volume of section \mathcal{B} is 1.00 L .

Calculate the work done by the gas in section \mathcal{A} . Calculate for the gas in each section: $\Delta \boldsymbol{U}$, q, $\Delta \boldsymbol{S}$, $\Delta \boldsymbol{A}$, $\Delta \boldsymbol{H}$, $\Delta \boldsymbol{G}$.

Calculate ΔS of the total system and its surroundings.

Assume $C_V = 20 \text{ J K}^{-1} \text{ mol}^{-1}$. Ideal: $C_p = 28.3144 \text{ J K}^{-1} \text{ mol}^{-1}$.

$$n = 2 \text{ moles}$$
 initial initial initial $T = 300 \text{ K}$ $V = 2 \text{ L}$ $V = 2 \text{ L}$ $p = ? = 24.6 \text{ atm}$ final final $T = ? \text{ K}$ $V = 2 \text{ L}$ $V = 2 \text{ L}$ $V = 2 \text{ L}$ final $V = ? = 3 \text{ L}$ $V = 1 \text{ L (given)}$ $V = 2 \text{ L}$ V

Work done on the gas in section \mathcal{B} $W_{\mathcal{B}} = -\int p_{op} \, dV \text{ (reversibly)} = -\int p_{gas} \, dV$ $= -\int nRT \, dV/V \qquad (p = nRT/V, \text{ ideal gas})$ $= -2 \times 8.3144 \times 300 \times \ln(1/2) = +3.46 \text{ kJ}$ $W_{\mathcal{A}} = -3.46 \text{ kJ}$

 $\Delta \textbf{\textit{U}},~q,~\Delta \textbf{\textit{S}},~\Delta \textbf{\textit{A}},~\Delta \textbf{\textit{H}},~{\rm and}~\Delta \textbf{\textit{G}}$:

	A	B
W_{rev}	- 3.46 kJ	+ 3.46 kJ
ΔU	ideal <i>U</i> = <i>U</i> (<i>T</i>)	ideal <i>U</i> = <i>U</i> (<i>T</i>)
	$\Delta U = \int C_V dT$	dT = 0
	=2×20×(900-300)	$\Delta U = 0$
	= 24 kJ	
q	$\Delta U = q + W$	$\Delta U = q + W$
	q = 27.46 kJ	q = -3.46 kJ
ΔS	$dS = (1/T)C_p dT$	$dS = (1/T)C_p dT$
	<i>- (∂V/∂T)_p</i> d <i>p</i>	- (∂V/∂T) _p dp
	$\Delta \mathbf{S} = n \int C_p \mathrm{d}T/T$	d <i>T=0</i>
	- n∫Rdp/p	$\Delta S = -n \int R dp/p$
	=2×28.3144×	= - 2×8.3144×
	In(900/300)	In(49.2/24.6)
	- 2×8.3144×	$= -11.53 \mathrm{J K^{-1}}$
	In(49.2/24.6)	
	$= +50.7 \mathrm{J K^{-1}}$	
ΔA	$\Delta \mathbf{A} = ?, dT \neq 0$	$\Delta A_T = W_{rev} =$
	≠ - 3.46 kJ	W_{max} = + 3.46 kJ

ΔH	ideal <i>H</i> = <i>H</i> (<i>T</i>)	ideal H = H (T)
	$\Delta \mathbf{H} = n \int C_p dT$	dT = 0
	= 2×28.3144×	∆ H = 0
	(900-300)	
	= 33.98 kJ	
∆G	$\Delta G = \Delta H - \Delta (TS)$	$\Delta G_T = \Delta H - T \Delta S$
	need to calculate	= - <i>T</i> ∆ S
	S at initial and	= 11.53×300 J
	final states	= 3.46 kJ

$$\Delta S_{\text{system}} = \Delta S_{A} + \Delta S_{B} = +50.7 - 11.53$$

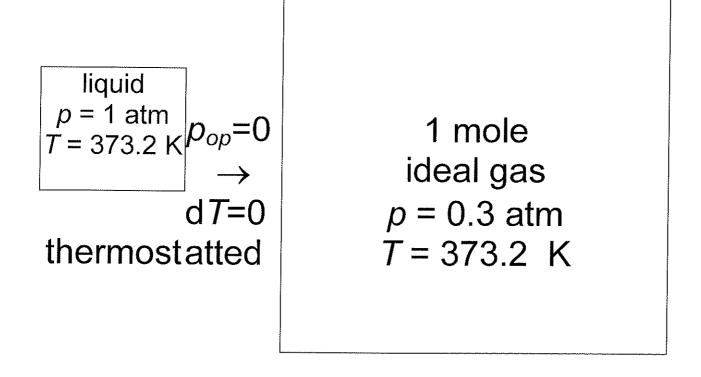
= +39.2 J K⁻¹

 $\Delta S_{\text{surrounding}} = -39.2 \text{ J K}^{-1}$ since process was carried out reversibly

EXAMPLE: 3 (b) One mole of liquid water (density = 1 g/mL) is allowed to expand into an evacuated flask of volume such that the final pressure is 0.3 atm. The bulb containing the liquid and the flask are thermostated so that a constant temperature of 100 °C is maintained. It is found that 11,000 cal of heat are absorbed when this process occurs. Calculate the values for ΔU , ΔH , ΔS , and ΔG . Assume vapor is ideal.

EXAMPLE: 3 (b) One mole of liquid water (density = 1 g/mL) is allowed to expand into an evacuated flask of volume such that the final pressure is 0.3 atm. The bulb containing the liquid and the flask are thermostated so that a constant temperature of 100 °C is maintained. It is found that 11,000 cal of heat are absorbed when this process occurs. Calculate the values for ΔU , ΔH , ΔS , and ΔG . Assume vapor is ideal.

Draw a Picture



$$\Delta U = ?$$
Given: $p_{op} = 0$ $q = 11,000$ cal $\partial W = p_{op} dV = 0$
∴ $\Delta U = q + W = 11,000$ cal

$$\Delta H = ?$$
 $H = U + pV$ $V_{liq} = 18 \times 10^{-3} \text{ L}$
 $\Delta H = \Delta U + \Delta (pV)$ $(pV)_{gas} = RT$
 $= 11,000 + [(pV)_{gas} - (pV)_{liq}]$
 $= 11,000 + [1.987 \times 373.2 - 18 \times 10^{-3} \times 1.987/0.082057]$
 $= 11,740 \text{ cal}$

```
\Delta S = ?
∆S is not 11000/373.2! not reversible
construct reversible steps leading to
liq, 1 atm, 373.2 K \rightarrowgas, 0.3 atm, 373.2
(a) liq, 1 atm, 373.2 \rightarrow gas, 1 atm, 373.2
(b) gas, 1 atm, \rightarrow gas, 0.3 atm,
                              373.2 K
          373.2 K
\Delta S = \Delta S_a + \Delta S_b \Delta H = \Delta H_a + \Delta H_b
use \int d\mathbf{S} = \hbar q_{rev}/T
          \mathsf{d}\mathbf{S} = (\partial \mathbf{S}/\partial T)_p \, \mathsf{d}T + (\partial \mathbf{S}/\partial p)_T \, \mathsf{d}p
            d\mathbf{S} = (C_p/T)dT - (\partial V/\partial T)_p dp
     (as derived in part a of this problem)
\Delta \mathbf{H}_b = \int (\partial \mathbf{H}/\partial T)_p \, dT + \int (\partial \mathbf{H}/\partial p)_T \, dp = 0 + 0
\Delta H = 11,740 = \Delta H_a + \Delta H_b = \Delta H_a + 0
\Delta S_a = q_{rev}/T = \Delta H_a/T = 11,740/373.2
\Delta S_b = \int (\partial V/\partial T)_p dp = -\int_1^{0.3} (R/p) dp
                               = -1.987 \ln (0.3/1)
\Delta S = 11740/373.2 + 1.987 \ln(1/0.3)
     = 33.85 cal K<sup>-1</sup>
```

$$\Delta S_{surr} = ?$$
 $\Delta S_{surr} = -11000/373.2 = -29.49$
 $\Delta S_{universe} = 33.85 - 29.49 = positive$
spontaneous change!

$$\Delta \boldsymbol{G} = \boldsymbol{?}$$
 $\Delta \boldsymbol{G}_T = \Delta \boldsymbol{H} - T\Delta \boldsymbol{S} = 11740 - 373.2 \times 33.85$
 $= 11740 - 12632.8 = -892.8 \text{ cal}$
or else
 $\Delta \boldsymbol{G} = \Delta \boldsymbol{G}_a + \Delta \boldsymbol{G}_b$
d $\boldsymbol{G} = Vdp - \boldsymbol{S}\underline{dT}$
(as derived in part a of this problem)
d $T = 0$ for all steps
 $\Delta \boldsymbol{G}_b = \int Vdp = \int_1^{0.3} (RT/p)dp$
 $= 1.987 \times 373.2 \times \ln(0.3/1) = -892.8 \text{ cal}$
 $\Delta \boldsymbol{G}_a = 0 \text{ gas and liq are at equilibrium}$
 $\Delta \boldsymbol{G} = -892.8 \text{ cal}$

$$\Delta A = ?$$

 $\Delta A = \Delta U - T \Delta S = 11000 - 12633 = -1633$
or $dA = -pdV - SdT \therefore -\int pdV = -1633$ cal

Maximum work = $W_{max} = W_a + W_b$ $W_a = -1 \int dV = -1 \{RT/1 - 18 \times 10^{-3} \text{ L}\}, \ p_{op} = 1$ = -740 cal $W_b = -\int p_{op} dV = -\int (RT/V) dV = -RT \ln(V_f/V_i)$ $(V_f/V_i) = [RT/0.3] \div [RT/1] = 1/0.3$ $W_b = -1.987 \times 373.2 \times \ln(1/0.3) = -892.8 \text{ cal}$ $W_{max} = -740 - 892.8 = -1633 \text{ cal} = -\int p dV$ $W_{max} = \Delta A_T = -1633 \text{ cal}$

An example of multiple approaches to a given problem:

Exam Problem 3(b) One mole of liquid water (density = 1 g/mL) is allowed to expand into an evacuated flask of volume such that the final pressure is 0.3 atm. The bulb containing the liquid and the flask are thermostated so that a constant temperature of 100 °C is maintained. It is found that 11,000 cal of heat are absorbed when this process occurs. Calculate the values for $\Delta \boldsymbol{U}$, $\Delta \boldsymbol{H}$, $\Delta \boldsymbol{S}$, and $\Delta \boldsymbol{G}$. Assume vapor is ideal.

dT = 0 for this system

	cal mol ⁻¹	from definition of the function	from relations derived from
			First and Second Law
ΔU	11,000	$q_{IRREV} + W_{IRREV} = 11,000 + 0$	$T\Delta S - \int p dV =$
		$q_{REV}+W_{REV}=12,633+-1633$	12,633 - 1633 = 11,000
		= 11,000	
$\Delta(pV)$	740	$p_f V_f - p_i V_i =$	
		RT - 1atm×0.018 L mol ⁻¹ =	
		741.2 - 0.436 ≈ 740	
ΔH	11,740	$\Delta U + \Delta(pV) =$	$T\Delta S + \int V dp =$
		11,000 + 740 = 11,740	12,633 - 843 = 11,740
T∆S	12,633	$q_{REV}=$	
		12,633	
ΔG	-893	$\Delta H - T \Delta S =$	$-\int \mathbf{S} dT + \int V dp =$
		11,740 - (12,633) = -893	0 + (-893) = -893
∫Vdp	-893		
$\int p dV$	1633	$-W_{REV}$	
∆ A		$\Delta U - T \Delta S =$	- ∫ <i>p</i> d <i>V</i> - ∫ S <u>d</u> <i>T</i> =
		11,000 - (12,633) = -1633	-1633 + 0 = -1633
۸.۵	22.97	a /T = 12.622/272 = 22.97	
$\Delta oldsymbol{\mathcal{S}}_{sys}$	33.87	$q_{REV}/T = 12,633/373 = 33.87$	
	cal mol ⁻¹	1	
	$ K^{-1} $	= 11740/373 - Rln(0.3/1) $= 21.47 + 2.20 = 22.86$	
	20.40	= 31.47 + 2.39 = 33.86	
$\Delta oldsymbol{S}_{surr}$	-29.49 	$(q_{REV})_{surr}/T = -11,000/373$	
		= -29.49	
	<u> </u>		

J			
	cal mol ⁻¹	from considering a function of two variables	
ΔU	11,000	$\Delta_{vap} \mathbf{U} = 11,000$ for phase change +	
		from $d\mathbf{U} = (\partial \mathbf{U}/\partial T)_V \underline{dT} + (\partial \mathbf{U}/\partial V)_T \underline{dV}$	
		= 0 +0	
		total = 11,000	
$\Delta(pV)$	740		
ΔH	11,740	$\Delta_{vap} \mathbf{H} = 11,740$ for phase change +	
		from $d\mathbf{H} = (\partial \mathbf{H}/\partial T)_p dT + (\partial \mathbf{H}/\partial p)_T dp$	
		= 0 +0	
TΔS	12,633		
$\Delta \mathbf{G}$	-893	Δ_{vap} G = 0 for phase change +	
		from $d\mathbf{G} = (\partial \mathbf{G}/\partial T)_p dT + (\partial \mathbf{G}/\partial p)_T dp$	
		$=$ $-\mathbf{S}dT + Vdp$	
		= $0 + (-893) = -893$	
∫ <i>V</i> d <i>p</i>	-893		
∫ <i>p</i> d <i>V</i>	1633	-W _{REV} {Note that ∆ A gives the maximum	
-		work done by the system}	
$\Delta \boldsymbol{A}$		$d\mathbf{A} = (\partial \mathbf{A}/\partial T)_V dT + (\partial \mathbf{A}/\partial V)_T dV$	
		$= -\int \mathbf{S} \underline{d} T - \int p dV$	
		= 0 - 1633 = -1633	
4.0	33.87	A 117 117 10 20 0 0 0 1	
$\Delta oldsymbol{S}_{sys}$	1 .	$\Delta_{vap}H/T=11740/373 + \text{for the next } rev \text{ step:}$	
	$ cal\ mol^{-1} $	$d\mathbf{S} = (\partial \mathbf{S}/\partial T)_{p} \underline{dT} + (\partial \mathbf{S}/\partial p)_{T} dp$	
	IV.	$= 0 - (\partial \mathbf{V}/\partial T)_p dp$	
		$= 0 - R \ln(0.3/1)$	
		= +2.39	
A C	20.40	total = 31.47+2.39 = 33.86	
$\Delta oldsymbol{S}_{surr}$	-47.47		