

Solutions to Problem Set 3

1. 1 mole liquid, T, 1 atm → vapor, T, 1 atm

Equation	Basis for the equation	Eq. #
$dU = (\partial U/\partial T)_V dT + (\partial U/\partial V)_T dV$	$U = U(T, V)$	1
$U(T, V) = f(T) - a/V$ $V_{\text{liquid}} = 18 \times 10^{-3} \text{ L mol}^{-1}$ $V_{\text{vapor}} = 24 \text{ L mol}^{-1}$ $a = 5.72 \text{ L}^2 \text{ atm mol}^{-1}$	Given	2
$U_{\text{liquid}} = f(T) - 5.72/18$ $U_{\text{vapor}} = f(T) - 5.72/24$ $U_{\text{vapor}} - U_{\text{liquid}} = -5.72/24 - (-5.72/0.018)$ $= 317.54 \text{ L atm mol}^{-1}$ $= 7690 \text{ cal mol}^{-1}$	substituting values of V into Eq 2	3 4 5
$H_{\text{vapor}} - H_{\text{liquid}} = U_{\text{vapor}} - U_{\text{liquid}} + p(V_{\text{vapor}} - V_{\text{liquid}})$ $= 317.54 + 1(24 - 0.018)$ $= 341.5 \text{ L atm mol}^{-1}$ $= 8270. \text{ cal mol}^{-1}$ <p style="text-align: right;">Answer</p> <p>This is smaller than $\Delta_{\text{vap}}H = 9820 \text{ cal mol}^{-1}$ expt</p>	$H = U + pV$ Definition Using Eq 5 and values of V	

2. 0.1 mol ideal monatomic gas $T_1 \rightarrow T_2$ along path $V = a \exp(bT)$

Equation	Basis for the equation	Eq. #
$p = 0.1RT/V$	Given ideal gas equation of state, 0.1 mol	1
$W = - \int p_{\text{op}} dV$	Definition	2
$p_{\text{op}} = p_{\text{gas}}$	given reversible	3
$W = - \int 0.1RT dV/V$		4
$V = a \exp(bT)$ $dV = a \exp(bT) \cdot b dT$ $dV/V = b dT$ $W = - \int 0.1RbT dT$ $W = -0.1 Rb(1/2)[T_2^2 - T_1^2]$ <p style="text-align: right;">Answer</p>	Given path Taking the ln Note the function for work depends on the path!	5 6 7 8 9
$q = C(T_2 - T_1)$ However, given it is an ideal gas, for which $(\partial U/\partial V)_T = 0$ $dU = (\partial U/\partial T)_V dT + (\partial U/\partial V)_T dV$ $dU = C_V dT$	Note that C is neither C_V nor C_p because the path is neither constant volume nor constant pressure. property of an ideal gas $U = U(T, V)$	10 11 12

$\Delta U = C_V[T_2 - T_1]$ $\Delta U = q + W, \quad q = \Delta U - W$ $q = C_V[T_2 - T_1]$ $+ (0.1Rb/2) \cdot [T_2^2 - T_1^2]$ Answer	First law of thermodynamics	13 14 15
$T_1 = 300 \text{ K} \quad T_2 = 400 \text{ K} \quad b = 0.01 \text{ K}^{-1}$	Given	16
$W = - (0.00831451/2)(400^2 - 300^2)$	Using Eq 9 and 0.1 mol	17
$W = - 291 \text{ J} = -0.291 \text{ kJ} \quad \textbf{Answer}$		18
$\Delta U = 1.5(8.31451)[400 - 300] = 1247 \text{ J}$ $= 1.247 \text{ kJ} \quad \textbf{Answer}$		19 20
$q = \Delta U - W = 1.538 \text{ J} \quad \textbf{Answer}$	Using Eq 14, 18 and 20	

3.

A

B

C

1 mole ideal gas $p_1, T_1, V_1 \rightarrow p_2, T_2, V_2 \rightarrow p_3, T_3, V_3 \rightarrow p_4, T_4, V_4$

A reversible heating at constant $p = 1 \text{ atm}$, from 298 to 373 K

B reversible isothermal expansion to $2V_2$

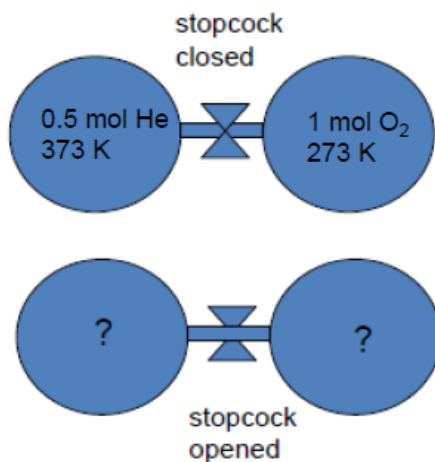
C reversible adiabatic cooling to 308 K

$C_p = (5/2)R$

Equation	Basis for the equation	Eq. #
$p_1 = 1 \text{ atm} \quad T_1 = 298$	Given ideal gas	1
$V_1 = R298/1 \text{ atm} = 24.45 \text{ L}$		2
$p_2 = 1 \text{ atm} \quad T_2 = 373$		3
$V_2 = R373/1 \text{ atm} = 30.61 \text{ L}$		4
$T_3 = T_2 = 373 \quad V_3 = 2V_2 = 61.22 \text{ L}$		5
$p_3 = R373/61.22 = 0.50 \text{ atm}$		6
$T_4 = 308 \text{ K}$		7
p_4, V_4 can be calculated but we actually do not need these		
$dU = C_V dT + (\partial U / \partial V)_T dV$	$U = U(T, V)$ and definition of C_V	8
$(\partial U / \partial V)_T = 0$	property of an ideal gas	9
$dU = C_V dT$		10
$dH = C_p dT + (\partial H / \partial p)_T dp$	$H = H(T, p)$ and definition of C_p	11
$(\partial H / \partial p)_T = 0$	property of an ideal gas	12
$dH = C_p dT$		13
Step A	From Eq 10 and given $C_V = (3/2)R$	14
$\Delta U = (3/2)R(373 - 298) = 935.4 \text{ J}$ Answer		
$\Delta H = (5/2)R(373 - 298) = 1559.0 \text{ J}$ Answer	From Eq 13 and given $C_p = C_V + R = (5/2)R$	15
$W = - \int p_{\text{op}} dV = -1 \text{ atm} [V_2 - V_1]$ $= -1 [30.61 - 24.45] = -6.16 \text{ L atm}$ $= -624.2 \text{ J}$ Answer	Definition and $p = \text{constant} = 1 \text{ atm}$	16 17

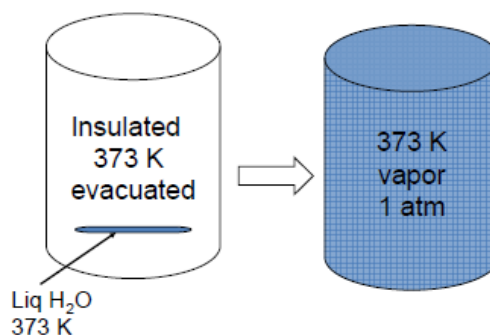
$dH = C_p dT + (\partial H / \partial p)_T dp$ $(\partial H / \partial p)_T = 0$ $\Delta H = C_p(373-298)$ Another way, $\Delta H = \Delta U + p_2 V_2 - p_1 V_1$ $= C_V(373-298) + R373 - R298$ $= C_p(373-298)$ the same	$H = H(T,p)$ and definition of C_p property of an ideal gas $H = U + pV$ definition Using ideal gas law $C_p - C_V = R$ for an ideal gas	6 7 8 9 10 11
Step B $W = - \int p_{op} dV$ $p_{op} = 0$ $W = 0$ $\Delta U = C_V dT = 0$ $\Delta U = q + W$ $q = \Delta U = 0$ $\Delta H = C_p dT = 0$	$dT = 0$ in a Joule expansion	12 13 14 15 16 17 18
Step C $q = C_p(298-373)$ $\Delta U = C_V(298-373)$ $\Delta U = q + W$ $W = C_V(298-373) - C_p(298-373)$ $= -R(298 - 373)$ Another way: $W = - \int p_{op} dV$ reversible $p_{op} = p_{gas}$ At constant pressure, $W = -p_3 \int dV = -p_3(V_4 - V_3) = -R298 - R373$ the same as $-R(298 - 373)$ found from first law $\Delta H = C_p(298 - 373)$.	19 20 21 22 23 24
for the overall process $q = C_V(373-298) + 0 + C_p(298-373)$ $= (C_p - C_V)298 - (C_p - C_V)373$ $q = R(298-373) = -0.624 \text{ kJ}$ <p style="text-align: right;">Answer</p> $W = 0 + 0 - R(298 - 373) = +0.624 \text{ kJ}$ <p style="text-align: right;">Answer</p> $\Delta U = C_V(373-298) + 0 + C_V(298-373)$ $\Delta U = 0$ Answer $\Delta H = C_p(373-298) + 0 + C_p(298-373)$ $\Delta H = 0$ Answer	$C_p - C_V = R$ for an ideal gas Note answers do not require C_p or C_V values.	

5. adiabatic process, ideal gases



Equation	Basis for the equation	Eq. #
$q=0$	Given adiabatic	1
$W = 0$	No work done to surroundings	2
$\Delta U = q + W = 0$		3
$dU = C_V dT + (\partial U / \partial V)_T dV$	$U = U(T, V)$ and Definition of C_V property of an ideal gas	4
$(\partial U / \partial V)_T = 0$		5
$\Delta U = C_V (T_f - T_i)$		6
$\Delta U_{He} = 0.5 (3/2) R (T_f - 373)$		7
$\Delta U_{O_2} = (5/2) R (T_f - 273)$		8
$0 = \Delta U_{He} + \Delta U_{O_2}$ $0 = 0.5(3/2)R(T_f - 373) + (5/2)R(T_f - 273)$ $T_f = \frac{(3/4)373 + (5/2)273}{(3/4) + (5/2)}$	From Eq 3 Solving for T_f	9
$T_f = 296 \text{ K}$ Answer		

6. 10 L tank, ideal gas vapor, negligible volume of liquid water



Equation	Basis for the equation	Eq. #
$q=0$	Given insulated, no q to or from surroundings	1
$W = 0$	vapor formed in evacuated volume	2
Final state: water vapor $V = 10 \text{ L}$, $T = 373$, $p = 1 \text{ atm}$ in equilibrium with remaining liquid		
$pV = nRT$ $1 \text{ atm} (10 \text{ L})$ $= n 0.0820578 \text{ L atm mol}^{-1} \text{ K}^{-1} (373)$ $n = 0.3267 \text{ mol}$	ideal gas	3 4
$\Delta H = 9720 \text{ cal mol}^{-1} (0.3267 \text{ mol})$ $= 3175 \text{ cal}$ Answer $\Delta U = q + W + U_{\text{vap}} - U_{\text{liq}} = \Delta_{\text{vap}} U$ $\Delta H = \Delta U + (pV)_{\text{vap}} - (pV)_{\text{liq}}$ $\Delta H = \Delta_{\text{vap}} U + 1 \text{ atm} (10 \text{ L}) - (\sim 0)$ $3175 \text{ cal} = \Delta_{\text{vap}} U$ $+ 1 \text{ atm} (10 \text{ L}) (1.9872 / 0.0820578)$ $\Delta_{\text{vap}} U = 3175 - 242.2 = 2933 \text{ cal}$ Answer	given $\Delta_{\text{vap}} H$ and using moles from Eq 4 first law $H = U + pV$ definition neglecting V_{liq} remaining in final state and neglecting $(pV)_{\text{liq}}$ at the initial state substituting value from Eq 5 into Eq 8 converting to cal from L atm	5 6 7 8

7. (a) 10 g ice(263 K) + 25 g liq water (288 K) \rightarrow ? adiabatic process

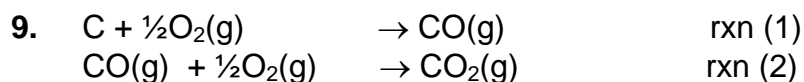
Equation	Basis for the equation	Eq. #
(i) 10 g ice(263 K) \rightarrow 10 g ice (273 K) (ii) 10 g ice(273 K) \rightarrow 10 g liq (273 K) (iii) 10 g liq(273 K) \rightarrow 10 g liq (T_f K) (iv) 25 g liq (288 K) \rightarrow 25 g liq (T_f K) $q = 0 = q_i + q_{ii} + q_{iii} + q_{iv}$ $q_i = 10 \text{ g} \cdot 0.5 \text{ cal K}^{-1} \text{ g}^{-1} \cdot (273 - 263) \text{ K}$ $q_{ii} = 10 \text{ g} \cdot 80 \text{ cal g}^{-1}$ $q_{iii} = 10 \text{ g} \cdot 1.0 \text{ cal K}^{-1} \text{ g}^{-1} \cdot (T_f - 273) \text{ K}$ $q_{iv} = 25 \text{ g} \cdot 1.0 \text{ cal K}^{-1} \text{ g}^{-1} \cdot (T_f - 288) \text{ K}$ $0 = 50 + 800 + 10T_f - 2730 + 25T_f - 7200$ Solving for T_f $T_f = 259.5 \text{ K}$ this answer is absurd .	One possibility is that all ice melts and final state is all liq water at $T_f \geq 273$. Another possibility is that only some of the ice melts and final state is some ice, some liquid water, all at 273 K The largest contribution comes from the q associated with melting of ice, so the second possibility is more likely. Nevertheless, let us try the first possibility and see what we find out. q contributions must sum to zero because it is an adiabatic process. $q = \int C dT$, and C is independent of temperature because it is lower than the freezing point of water. Therefore it is not possible that all ice melts	

<p>(i) 10 g ice(263 K) \rightarrow 10 g ice (273 K) (ii) x g ice(273 K) \rightarrow x g liq (273 K) (iiii) 25 g liq(288 K) \rightarrow 25 g liq (273 K) $q = 0 = q_i + q_{ii} + q_{iii}$ $q_i = 10\text{g} \cdot 0.5 \text{ cal K}^{-1} \text{g}^{-1} \cdot (273-263)\text{K}$ $q_{ii} = x \text{ g} \cdot 80 \text{ cal g}^{-1}$ $q_{iii} = 25 \text{ g} \cdot 1.0 \text{ cal K}^{-1} \text{g}^{-1} \cdot (273-288)\text{K}$</p> <p>$0 = 50 + 80x - 375$ $x = 4.06 \text{ g of ice melted}$ Final state is 5.94 g ice 29.06 g liq water all at 273 K Answer</p>	<p>Assume only some of the ice melts and the final state is some ice some liquid all at 273 K</p> <p>q contributions must sum to zero because it is an adiabatic process</p> <p>solve for x</p>
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Equation	Basis for the equation	Eq. #
(i) 10 g ice(263 K) \rightarrow 10 g ice (273 K)	One possibility is that all ice melts and final state is all liq water at $T_f \geq 273$. Another possibility is that only some of the ice melts and final state is some ice, some liquid water, all at 273 K Let us try the first possibility and see what we find out. Adiabatic process	1
(ii) 10 g ice(273 K) \rightarrow 10 g liq (273 K)		2
(iii) 10 g liq(273 K) \rightarrow 10 g liq (T_f K)		3
(iv) 100 g liq (288 K) \rightarrow 100 g liq (T_f K)		4
$q = 0 = q_i + q_{ii} + q_{iii} + q_{iv}$		5
$q_i = 10\text{g} \cdot 0.5 \text{ cal K}^{-1} \text{g}^{-1} \cdot (273-263)\text{K}$		6
$q_{ii} = 10 \text{ g} \cdot 80 \text{ cal g}^{-1}$		7
$q_{iii} = 10 \text{ g} \cdot 1.0 \text{ cal K}^{-1} \text{g}^{-1} \cdot (T_f - 273)\text{K}$		8
$q_{iv} = 100 \text{ g} \cdot 1.0 \text{ cal K}^{-1} \text{g}^{-1} \cdot (T_f - 288)\text{K}$		9
$0 = 50 + 800 + 10T_f - 2730$ $\quad\quad\quad + 100T_f - 28800$	Substituting each term into Eq 5	10
Solving for T_f		
$T_f = 278.9 \text{ K}$		
The final state is 110 g liquid water at 278.9 K		
Answer		

Equation	Basis for the equation	Eq. #
(a) Final products are equimolar $\text{CO(g)} + \text{H}_2\text{(g)}$ Combustion at 298 K, 1 atm: $\text{CO(g)} + \text{H}_2\text{(g)} + \text{O}_2 \rightarrow \text{CO}_2\text{(g)} + \text{H}_2\text{O(g)}$ $\Delta_{\text{rxn}} \mathbf{H} = \Delta_{\text{form}} \mathbf{H}[\text{CO}_2\text{(g)}] + \Delta_{\text{form}} \mathbf{H}[\text{H}_2\text{O(g)}]$ $\quad - \Delta_{\text{form}} \mathbf{H}[\text{CO(g)}]$	Assuming only rxn (1) occurs Given Assuming all combustion products are vapor By definition, $\Delta_{\text{form}} \mathbf{H}[\text{H}_2\text{(g)}] = 0$ $\Delta_{\text{form}} \mathbf{H}[\text{O}_2\text{(g)}] = 0$	1 2 3

$\Delta_{\text{rxn}}H = -393.51 - 241.82 - (-110.53)$ $= -524.8 \text{ kJ mol}^{-1}$	Look up $\Delta_{\text{form}}H$ for $\text{CO}_2(\text{g})$, $\text{H}_2\text{O}(\text{g})$ and $\text{CO}(\text{g})$ in textbook at 1 atm, 298 K in kJ mol^{-1}	4
For 1 L of water gas $pV = nRT$ $n = 1 \text{ atm} \cdot 1 \text{ L}$ $/(0.0820578 \text{ L atm mol}^{-1} \text{ K}^{-1} \cdot 298)$ $n = 0.0409 \text{ mol} = 0.02045 \text{ mol CO}$ $+ 0.02045 \text{ mol H}_2$ $\Delta_{\text{comb}}H$ of 1 L of water gas $= 0.02045 \text{ mol} \cdot (-524.8 \text{ kJ mol}^{-1})$ $= -10.73 \text{ kJ}$ Answer	Assume ideal behavior Ideal gas law Solve for total number of moles in 1 L of gas for this number of moles	5 6 7 8
(b) Final products of water gas reaction are $0.95 \text{ CO}(\text{g}) + 0.05 \text{ CO}_2(\text{g}) + 1.05 \text{ H}_2(\text{g})$ For 1 L of water gas, $n = 0.0409 \text{ mol}$ as before, $= 0.01895 \text{ mol CO} + 0.0010 \text{ mol CO}_2$ $+ 0.02095 \text{ mol H}_2$ $\text{CO}(\text{g}) + \frac{1}{2}\text{O}_2 \rightarrow \text{CO}_2(\text{g})$ $\Delta_{\text{rxn}}H = \Delta_{\text{form}}H[\text{CO}_2(\text{g})] - \Delta_{\text{form}}H[\text{CO}(\text{g})]$ $= -393.51 - (-110.53)$ $= -282.98 \text{ kJ mol}^{-1}$ $\text{H}_2(\text{g}) + (1/2)\text{O}_2 \rightarrow \text{H}_2\text{O}(\text{g})$ $\Delta_{\text{rxn}}H = \Delta_{\text{form}}H[\text{H}_2\text{O}(\text{g})]$ $= -241.82 \text{ kJ mol}^{-1}$ $\Delta_{\text{comb}}H$ of 1 L of water gas $= 0.01895 \text{ mol} \cdot -282.98 \text{ kJ mol}^{-1}$ $+ 0.02095 \text{ mol} \cdot -241.82 \text{ kJ mol}^{-1}$ $= -10.42 \text{ kJ}$ Answer	95% of C appears as CO from rxn (1) and and 5% as CO_2 from rxn (2) but now consists of $(0.95/2.05)(0.0409) \text{ mol CO}$ $+ (0.05/2.05)(0.0409) \text{ mol CO}_2$ $+ (1.05/2.05)(0.0409) \text{ mol H}_2$ Do $\Delta_{\text{rxn}}H$ separately because no longer 1:1 in CO and H_2 Using $\Delta_{\text{form}}H$ for $\text{CO}_2(\text{g})$ and $\text{CO}(\text{g})$ Using $\Delta_{\text{form}}H$ for $\text{H}_2\text{O}(\text{g})$ Using the number of moles found in Eq 10 Enthalpy of combustion of 1 L of water gas	9 10 11 12



Equation	Basis for the equation	Eq. #
Final products are 0.95 mol CO + 0.05 mol CO_2 for every 0.5 mol O_2 used up, which is accompanied by 2.0 mol N_2 in the dry air used to produce the gas	95% of O_2 appears in CO from rxn (1) and and 5% in CO_2 from rxn (2)	
consider 1 L producer gas at 1 atm $pV = nRT$ $n = 1 \text{ atm} \cdot 1 \text{ L}$ $/(0.0820578 \text{ L atm mol}^{-1} \text{ K}^{-1} \cdot 298)$ $n = 0.0409 \text{ mol}$ $= (0.95/3.0)(0.0409) \text{ mol CO} + .$	Ideal gas law	1 2 3

(0.05/3.0)(0.0409 mol CO ₂ + (2.0/3.0)(0.0409) mol N ₂ or 0.01295 mol CO	Of the components only CO can contribute to heating value	
Combustion of CO in air CO(g) + ½O ₂ (g) → CO ₂ (g) Δ _{rxn} H = Δ _{form} H[CO ₂ (g)] - Δ _{form} H[CO(g)] = -393.51 - (-110.53) = -282.98 kJ mol ⁻¹	By definition, Δ _{form} H[O ₂ (g)] = 0 using Δ _{form} H for CO ₂ (g) and CO(g) in textbook at 1 atm, 298 K in kJ mol ⁻¹	4 5 6
Δ _{comb} H = 0.01295 mol • -282.98 kJ mol ⁻¹ = 3.66 kJ per L of producer gas Answer	For 1 L producer gas containing 0.01295 mol CO	7

10. (a) CH₄(g) + 2O₂(g)/air at 293 K → CO₂(g) + 2H₂O(g) at 373 K

Equation	Basis for the equation	Eq. #
1 mol CH ₄ 4 mol O ₂ 16 mol N ₂	given Twice the minimum amount of air is used for combustion	
At 293 K CH ₄ (g) + 2O ₂ (g) → CO ₂ (g) + 2H ₂ O(l) Δ _{comb} H = -212.91 kcal mol ⁻¹	Definition of Δ _{comb} H is that products of combustion are CO ₂ (g) and H ₂ O(l) Given	1 2
CO ₂ (g) 293 K → CO ₂ (g) 373 K (1) 2H ₂ O (l) 293 K → 2H ₂ O (l) 373 K (2) 2H ₂ O (l) 373 K → 2H ₂ O (g) 373 K (3) 16N ₂ (g) 293 K → 16N ₂ (g) 373 K (4) <u>2O₂(g) 293 K → 2O₂(g) 373 K (5)</u> CH ₄ (g) + 4O ₂ (g) + 16N ₂ (g) at 293 K → CO ₂ (g) + 2H ₂ O(g) + 2O ₂ + 16N ₂ at 373 K	The CO ₂ product has to be heated to 373 K the liquid water has to be heated to 373 K and vaporized The N ₂ and the unused O ₂ have to be heated to 373 K Adding up the changes	3 4 5 6 7 8
ΔH = Δ _{comb} H + ΔH(1) + ΔH(2) + ΔH(3) + ΔH(4) + ΔH(5) ΔH(1) = 1 • 8.87 cal mol ⁻¹ K ⁻¹ (373-293) ΔH(2) = 2 • 18 cal mol ⁻¹ K ⁻¹ (373-293) ΔH(3) = 2 • 9720 cal mol ⁻¹ ΔH(4) = 16 • 6.96 cal mol ⁻¹ K ⁻¹ • (373-293) ΔH(5) = 2 • 7.02 cal mol ⁻¹ K ⁻¹ (373-293)	Using dH = C _p dT at dp = 0 Using Δ _{vap} H = 9720 cal mol ⁻¹ for water	9 10 11 12 13 14
ΔH = -212.91 × 10 ³ + 709.6 + 2880 + 19440 + 8909 + 1123 = -179848 cal Answer	Summing up terms in Eq 9 from Eq 10-14 heat liberated for 1 mol of CH ₄ gas burned	

10. (b) $\text{CH}_4(\text{g}) + 2\text{O}_2(\text{g})/\text{air}$ at 293 K \rightarrow $\text{CO}_2(\text{g}) + 2\text{H}_2\text{O}(\text{g})$ at T K

Equation	Basis for the equation	Eq. #
1 mol CH_4 4 mol O_2 16 mol N_2	given Twice the minimum amount of air is used for combustion	
final state of stack gases: T such that saturated with water vapor but no condensation Composition of stack gases: 2 mol O_2 + 16 mol N_2 + 1 mol CO_2 + 2 mol H_2O = 21 mol $x_{\text{H}_2\text{O}} = 2/21 = 0.095$ 0.095 atm is the partial pressure of water at 1 atm total pressure or 72 mm Hg	given find the mole fraction of water in the stack gases using plot of vapor pressure of water, 72 mm Hg corresponds to 40°C or 313 K	2 3
same steps Eq 3-8 as in 10.(a) have to be added up except T is 313 not 373	Everything is the same as in 10. (a) except that the temperature of the stack gases is 313 K instead of 373 K and we need to get $\text{H}_2\text{O}(\text{g})$ from 373 K back down to 313 K	
$\Delta H = \Delta_{\text{comb}} H + \Delta H(1) + \Delta H(2) + \Delta H(3) + \Delta H(2a) + \Delta H(4) + \Delta H(5)$ $\Delta H(1) = 1 \cdot 8.87 \text{ cal mol}^{-1} \text{ K}^{-1} (313-293)$ $\Delta H(2) = 2 \cdot 18 \text{ cal mol}^{-1} \text{ K}^{-1} (373-293)$ $\Delta H(3) = 2 \cdot 9720 \text{ cal mol}^{-1}$ $\Delta H(2a) = 2 \cdot 8.03 \text{ cal mol}^{-1} \text{ K}^{-1} (313-373)$ $\Delta H(4) = 16 \cdot 6.96 \text{ cal mol}^{-1} \text{ K}^{-1} \cdot (313-293)$ $\Delta H(5) = 2 \cdot 7.02 \text{ cal mol}^{-1} \text{ K}^{-1} (313-293)$	Using $dH = C_p dT$ at $dp = 0$ Using $\Delta_{\text{vap}} H = 9720 \text{ cal mol}^{-1}$ for water at 373 K	4 5 6 7 8 9 10
$\Delta H = -212.91 \times 10^3 + 177 + 2880 + 19440 - 321 + 2227 + 280$ $= -188227 \text{ cal}$ Answer	Summing up Eq 5-10 into Eq 4 heat liberated for 1 mol of CH_4 gas burned to stack gases at 313 K where water in saturated vapor just fails to condense	