

Solutions to Problem Set 5

1. ideal gas, 1 mol 1 L 25 °C → 100 L 25 °C

Equation	Basis for the equation	Eq. #
$dU = (\partial U/\partial T)_V dT + (\partial U/\partial V)_T dV$	$U = U(T, V)$	1
$dH = (\partial H/\partial T)_p dT + (\partial H/\partial p)_T dp$	$H = H(T, p)$	2
$\Delta U = 0$ Answer	For an ideal gas, $(\partial U/\partial V)_T = 0$ and $(\partial H/\partial p)_T = 0$ and $dT = 0$ for this problem	3
$\Delta H = 0$ Answer		4
$dS = (\partial S/\partial T)_V dT + (\partial S/\partial V)_T dV$	$S = S(T, V)$	5
$(\partial S/\partial V)_T = (\partial p/\partial T)_V$	Derived (see lecture notes Part 4) starting from $dU = \delta q_{rev} - p dV = T dS - p dV$ and use of cross derivatives	6
$p = RT/V$	Ideal gas equation of state for one mol Differentiating Substituting Eq 8 into Eq 6	7
$(\partial p/\partial T)_V = R/V$		8
$(\partial S/\partial V)_T = R/V$		9
$\Delta S = \int (R/V) dV$	Substituting Eq 9 into Eq 5 and using $dT = 0$ for this problem	10
$\Delta S = R \ln(V_f/V_i)$ $= (1 \text{ mol})(8.314 \text{ J mol}^{-1} \text{ K}^{-1}) \bullet \ln(100/1) = 38.3 \text{ J K}^{-1}$ Answer	Integrating Eq 10 between the limits	11
$A = U - TS$	Definition	12
$\Delta A = \Delta U - T \Delta S$	At constant T	13
$\Delta A = 0 - (298)(38.3 \text{ J K}^{-1})$ $\Delta A = -11409. \text{ J}$	From $\Delta U = 0$ Eq 3 & ΔS from Eq 11, and given $T = 298 \text{ K}$	14
$G = H - TS$	Definition	12
$\Delta G = \Delta H - T \Delta S$	At constant T	13
$\Delta G = 0 - (298)(38.3 \text{ J K}^{-1})$ $\Delta G = -11409. \text{ J}$	From $\Delta H = 0$ Eq 4 & ΔS from Eq 11, and given $T = 298 \text{ K}$	14

2. (a) ideal gas, 1 mol 22.4 L, 0 °C → 224 L, 0 °C isothermal, reversible

Equation	Basis for the equation	Eq. #
$\Delta U = 0$ Answer $\Delta H = 0$ Answer $\Delta S = R \ln(V_f/V_i)$ $= (1 \text{ mol})(8.314 \text{ J mol}^{-1} \text{ K}^{-1}) \bullet \ln(224/22.4) = 19.14 \text{ J K}^{-1}$ Answer $\Delta A = - (273)(19.1 \text{ J K}^{-1})$ $= -5226 \text{ J}$ Answer $\Delta G = - (273)(19.1 \text{ J K}^{-1})$ $= -5226 \text{ J}$ Answer	Using all the same equations as in problem 1 (Eq 1-14) except for $V_f = 224 \text{ L}$ and $V_i = 22.4 \text{ L}$, $T = 273 \text{ K}$. Reversible or otherwise, the same equations hold for state functions for isothermal process for ideal gas.	

$\delta W = -p_{op}dV$	Definition of pV work	1
$p_{op} = p_{gas}$	reversible	2
$p_{gas} = (1)RT/V$	ideal gas equation of state, 1 mole	3
$\delta W = -RTdV/V$ $W = -\int RTdV/V = -(1 \text{ mol})(8.314 \text{ J mol}^{-1}\text{K}^{-1})273 \cdot \ln(224/22.4)$ $= -5226 \text{ J}$ Answer	From Eq 1, 2 and 3 Integrating	4
$dU = \delta q + \delta W$	First Law of Thermodynamics	5
$\Delta U = 0$	Already found	
$0 = q + W$ $q = -W = +5226 \text{ J}$ Answer	From Eq 5 This is q for the system	6
$\Delta S_{surr} = -5226 \text{ J} / 273 \text{ K} = -19.14 \text{ J K}^{-1}$ $\Delta S_{universe} = \Delta S_{gas} + \Delta S_{surr} = 19.14 - 19.14 = 0 \text{ J K}^{-1}$ as expected for a reversible process Answer	q for the surroundings is – 5226 J and T = 273	7

(b) ideal gas, 1 mol 22.4 L, 0 °C → 224 L, 0 °C irreversible expansion into evacuated vessel

Equation	Basis for the equation	Eq. #
$\Delta U = 0$ $\Delta H = 0$ $\Delta S = 19.14 \text{ J K}^{-1}$ $\Delta A = -5226 \text{ J}$ $\Delta G = -5226 \text{ J}$ Answer	The same values hold for changes in state functions <i>for identical initial and final states</i> , regardless of the process that brought it about.	1
$\delta W = -p_{op}dV$	Definition of pV work	2
$p_{op} = 0$	Expanding into a vacuum, the gas encounters zero opposing pressure	3
$W = 0$ Answer	Since $p_{op} = 0$	4
$dU = \delta q + \delta W$	First law of thermodynamics	5
$q = 0$ Answer	From Eq 4 and 5	6
$q_{surroundings} = 0$	Since no heat passed between gas and its surroundings	7
$\Delta S_{surr} = 0$	Can imagine a reversible process by which the surroundings accepted zero heat from the gas at 0 °C	8
$\Delta S_{universe} = \Delta S_{gas} + \Delta S_{surr}$ $= 19.14 \text{ J K}^{-1}$	$\Delta S_{universe}$ is positive, consistent with a spontaneous expansion of a gas into vacuum	9

3. ideal gas, 1 mol $V_1, T_1 \rightarrow V_2, T_2$ irreversible adiabatic expansion no work done

Equation	Basis for the equation	Eq. #
$W = 0$	Given	1
$q = 0$	Given (adiabatic)	2
$dU = \delta q + \delta W$	First law of thermodynamics	3
$\Delta U = 0$	From Eq 1, 2 and 3	4
$dU = (\partial U/\partial T)_V dT + (\partial U/\partial V)_T dV$	$U = U(T, V)$	5
$\Delta U = \int C_V dT$	For an ideal gas, $(\partial U/\partial V)_T = 0$	6
$dT = 0$ Answer	Since $\Delta U = 0$ and C_V cannot be zero This is a consequence of the condition that no work is done by the gas.	7
$dS = (\partial S/\partial T)_V dT + (\partial S/\partial V)_T dV$ $(\partial S/\partial V)_T = (\partial p/\partial T)_V$ $(\partial p/\partial T)_V = R/V$ $(\partial S/\partial V)_T = R/V$ $\Delta S = \int (R/V) dV$	Using the same arguments as in the previous problem for 1 mole of an ideal gas undergoing a volume change and also $dT = 0$	8
$\Delta S = R \ln (V_2/V_1)$	This is positive since $V_2 > V_1$ in an expansion	
$q_{\text{surroundings}} = 0$	Since no heat passed between gas and its surroundings	7
$\Delta S_{\text{surr}} = 0$	Can imagine a reversible process by which the surroundings accepted zero heat from the gas at T_1	8
$\Delta S_{\text{universe}} = \Delta S_{\text{gas}} + \Delta S_{\text{surr}}$ $= R \ln (V_2/V_1)$	$\Delta S_{\text{universe}}$ is positive, consistent with an irreversible process for the gas	9
$\Delta S_{\text{gas}} = R \ln(V_2/V_1)$ since $dT=0$, ideal gas $\Delta U = 0$, $q = -W$ $W = - \int RT dV/V = - RT \ln(V_2/V_1)$ $q_{\text{gas}} = RT \ln(V_2/V_1)$ $q_{\text{surroundings}} = - RT \ln(V_2/V_1)$ $\Delta S_{\text{surr}} = -R \ln(V_2/V_1)$ $\Delta S_{\text{universe}} = \Delta S_{\text{gas}} + \Delta S_{\text{surr}} = 0$ as expected for a reversible process	<i>If on the other hand, reversible isothermal process for 1 mol ideal gas from V_1 to V_2, then conditions are the same as in Problem 2 and $q = -W$ where W can be calculated from $p_{\text{op}} = p_{\text{gas}}$ leading to $q_{\text{surroundings}}/T$ opposite sign to ΔS_{gas}</i>	10

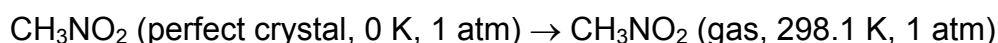
4. ideal gas 1 mol in contact with heat reservoir at 25°C 100 atm $\rightarrow$ 1 atm

Equation	Basis for the equation	Eq. #
$dS = (\partial S/\partial T)_p dT + (\partial S/\partial p)_T dp$	$S = S(T, p)$	1
$(\partial S/\partial p)_T = -(\partial V/\partial T)_p$	Derived (see lecture notes Part 4) starting from $dU = \delta q_{\text{rev}} - p dV = T dS - p dV$ and use of cross derivatives	2

$V = RT/p$ $(\partial V/\partial T)_p = R/p$ $(\partial S/\partial p)_T = -R/p$	Ideal gas equation of state for one mol Differentiating Substituting Eq 4 into Eq 2	3 4 5
$\Delta S = - \int (R/p) dp$	Substituting Eq 5 into Eq 1 and using $dT = 0$ for this problem	6
$\Delta S_{\text{gas}} = - (1 \text{ mol})(8.314 \text{ J mol}^{-1}\text{K}^{-1}) \bullet \ln(1/100) = + 38.3 \text{ J mol}^{-1}\text{K}^{-1}$	In all cases, for the same initial and final conditions, regardless of whether work is done or not during the process, because S is a state function	7
$\Delta U = 0, \Delta U = q + W$	Ideal gas and first law of thermodynamics	8
$q_{\text{system}} = - W_{\text{system}}$	In all cases, for the same initial and final conditions, regardless of whether work is done or not during the process, because U is a state function and the first law of thermodynamics always holds.	
$q_{\text{surr}} = - q_{\text{system}} = W_{\text{system}}$	Any heat transferred from the system goes into the surroundings. q_{surr} is negative (the surroundings provide heat to the system) when the gas does some work	

	W_{system}	q_{surr}	$\Delta S_{\text{surr}} = q_{\text{surr}}/T$	ΔS_{gas}	$\Delta S_{\text{universe}} = \Delta S_{\text{surr}} + \Delta S_{\text{gas}}$
(a)	- 2730 cal = - 11422 J	- 11422 J	-11422/298 = - 38.3 J K ⁻¹	+38.3 J K ⁻¹	0
(b)	- 1000 cal = -4184 J	- 4184 J	-4184/298 = - 14.0 J K ⁻¹	+38.3 J K ⁻¹	+24.3 J K ⁻¹
(c)	0 cal	0 J	0	+38.3 J K ⁻¹	+38.3 J K ⁻¹

5. Third law entropy of CH₃NO₂ (gas, 298.1 K, 1 atm) can be obtained by adding up the entropies for all the transformations needed for



We will use

$$dS = (\partial S/\partial T)_p dT + (\partial S/\partial p)_T dp = (C_p/T) dT - (\partial V/\partial T)_p dp$$

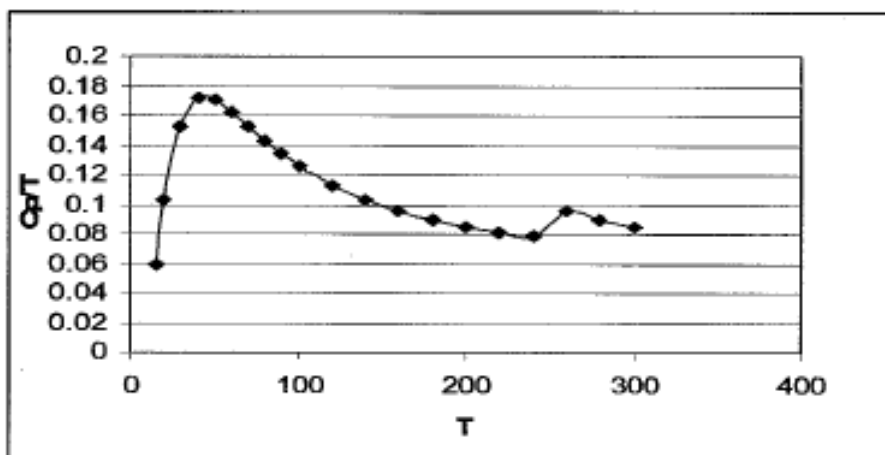
$$(\partial S/\partial p)_T = -(\partial V/\partial T)_p$$

$$dS = (C_p/T) dT - (\partial V/\partial T)_p dp$$

Since $p = 1 \text{ atm}$, $dp = 0$, $dS = (C_p/T) dT$; $\Delta S = \int (C_p/T) dT$

For a phase transformation where $dT = 0$, we will use $\Delta S = q_{\text{REV},p}/T_{\text{trans}} = \Delta H_{\text{trans}}/T_{\text{trans}}$

Given the table of C_p (cal mol⁻¹ K⁻¹) as function of T , calculate C_p/T values and plot vs T to find the integral of $(C_p/T) dT$ between 15 K and 298.1 K



CH ₃ NO ₂ (perfect crystal, 0 K, 1 atm)	S = 0 at absolute 0 K for a perfect crystal (Third law of thermodynamics)	0
(crystal, 15 K, 1 atm)	for dp = 0 $\Delta S_1 = \int_0^{15} (C_p/T) dT$ For solids, C _p and C _v are nearly the same $C_p - C_v = -T \left(\frac{\partial V}{\partial T} \right)_p^2 \left(\frac{\partial p}{\partial V} \right)_T$ because the two factors are small for solids, especially for low T. For perfect solids, C _v behaves asymptotically $\lim_{(T \rightarrow 0 \text{ K})} C_v = aT^3$ $C_v = 464.4(T/\Theta_D)^3 \text{ cal mol}^{-1} \text{ K}^{-1} = aT^3$ where $\Theta_D = 215 \text{ K}$ for Cu, for example, therefore $a = 4.67 \times 10^{-5}$ Debye extrapolation from 0 K to 15K Debye: $\Delta S_1 = (1/3)a(15)^3 = 0.05 \text{ cal mol}^{-1} \text{ K}^{-1}$ This seems rather small.	ΔS_1
(crystal, 244.7 K, 1 atm)	Integration from 15K to 244.7 K, dp = 0 (ΔS_2) Integration over the whole range of temperatures 15K to 298.1 K gives $30.52 \text{ cal mol}^{-1} \text{ K}^{-1}$ which includes ($\Delta S_2 + \Delta S_4$)	ΔS_2
(liquid, 244.7 K, 1 atm)	Phase transition at 244.7 K $\Delta H = q_{p, \text{REV}} = 2319 \text{ cal mol}^{-1}$ $\Delta S_3 = 2319 \text{ cal mol}^{-1} / 244.7 \text{ K} = 9.48 \text{ cal mol}^{-1} \text{ K}^{-1}$	ΔS_3
(liquid, 298.1, 1 atm)	Integration from 244.7 K to 298.1 K, dp = 0 (ΔS_4) This is already included in ($\Delta S_2 + \Delta S_4$) integration.	ΔS_4
(liquid, 298.1, 3.666 cm Hg)	Integration from 76.0 cm Hg to 3.666 cm Hg at 298.1 K for liquid, dT = 0 For the liquid, assume small temperature coefficient of volume, $(\partial V/\partial T)_p \sim 0$, leads to $(\partial S/\partial p)_T = -(\partial V/\partial T)_p$	ΔS_5

	~ 0 $\Delta S_5 = 0$	
(vapor, 298.1, 3.666 cm Hg)	Phase transition at 298.1 K, 3.666 cm Hg $\Delta S_6 = 9147 \text{ cal mol}^{-1} / 298.1 \text{ K} = 30.68 \text{ cal mol}^{-1} \text{ K}^{-1}$	ΔS_6
(vapor, 298.1, 1 atm)	Integration from 3.666 cm Hg to 76.0 cm Hg at 298.1 K for gas, $dT = 0$ For the vapor, if ideal: $V = RT/p$ $(\partial V / \partial T)_p = R/p$ $(\partial S / \partial p)_T = -R/p$ $\Delta S_7 = -R \ln(76.0/3.666) = -6.03 \text{ cal mol}^{-1} \text{ K}^{-1}$	ΔS_7
$S_{\text{absolute}} = 65.70 \text{ cal mol}^{-1} \text{ K}^{-1}$ Answer	$S_{\text{absolute}} =$ $S(0 \text{ K}) + \Delta S_1 + \Delta S_2 + \Delta S_3 + \Delta S_4 + \Delta S_5 + \Delta S_6 + \Delta S_7$	

6. N_2 gas at 1000 atm, 1000 °C fugacity = ?

Equation	Basis for the equation	Eq. #
$\ln \frac{f}{p} = \int_0^p \frac{(Z-1)}{p} dp$	Relation of fugacity to pressure (from lecture notes Part 5)	1
$Z = pV/RT$	For a non-ideal gas, Z is not 1	2
$p(V-b) = RT$ $b = 39.1 \times 10^{-3} \text{ L mol}^{-1}$	Equation of state to be used for this gas	3
$Z = V/(V-b)$	From Eq 2 and 3	4
$Z-1 = b/(V-b)$		5
$(Z-1)/p = b/RT$	From Eq 3 and 5	6
$\int (Z-1) dp/p = (b/RT) \int_0^p dp$	From Eq 6	7
$\ln (f/p) = (b/RT)p$	From Eq 1 and 7	8
$f = p \cdot \exp(bp/RT)$	Eq 8 and definition of ln	9
$f = 1000 \text{ atm} \cdot \exp[0.0391 \text{ L mol}^{-1} \cdot 1000 \text{ atm} / (0.08205 \text{ L atm mol}^{-1} \text{ K}^{-1} \cdot 1273 \text{ K})] = 1450 \text{ atm}$ Answer	Substituting values into Eq 9 and evaluating	

7. From given table of Z vs p, calculate the following:

p	1.0000	4.00000	7.00000	10.0000	40.0	70.0	100.0
(Z-1)/p	-0.00290	-0.00301	-0.00303	-0.00304	-0.00316	-0.00319	-0.00313

Equation	Basis for the equation	Eq. #
$\ln \frac{f}{p} = \int_0^p \frac{(Z-1)}{p} dp$	Relation of fugacity to pressure (from lecture notes Part 5)	1
$(Z-1)/p = -0.0031 - 2 \times 10^{-6} (p/1\text{atm})$	Fit the values in above table to a function of p. Nearly independent of p.	2

$\ln(f/p) = \text{Integral} \approx -0.31$	Integral = area under this curve for $p = 0$ to $p=100$ atm has a value very close to $100 \bullet (-0.0031)$	3
$f = p \exp(-0.31) = 0.733p$ $f = 73.3 \text{ atm at } 100 \text{ atm, } 200 \text{ K}$ Answer	From Eq 3 rearrange and evaluate	

8.

Equation	Basis for the equation	Eq. #
$dG = Vdp - SdT$	One of the four fundamental equations of thermodynamics	1
$dG = (\partial G/\partial T)_p dT + (\partial G/\partial p)_T dp$	$G = G(T,p)$	2
$(\partial G/\partial p)_T = V$	From Eq 1 & 2	3
$G = RT \ln(p/1\text{atm}) + A' + B'p + (1/2)C'p^2 + (1/3)D'p^3$	Given $G = G(T,p)$ functional form	4
$V = RT/p + B' + C'p + D'p^2$ This is the equation of state Answer	Taking $(\partial G/\partial p)_T$ and equating it to V	5

9. At 100 °C and 1 atm, water and steam are at equilibrium (this point is on the liquid-vapor equilibrium curve for H₂O):

water (100 °C and 1 atm) $\Leftrightarrow$ steam (100 °C and 1 atm)

Equation	Basis for the equation	Eq. #
$H = U + pV$	Definition	1
$dU = \delta q + \delta W$	First law of thermodynamics	2
$\Delta U = q_p - p\Delta V$ $\Delta H = \Delta U + p\Delta V$	At constant opposing pressure p	3
$\Delta H = q_p$	At constant pressure, from 3	4
$\Delta S = q_{\text{REV}}/T$	Second law of thermodynamics	5
$\Delta S = \Delta H/T$	q_{REV} is also q_p at constant pressure (1 atm) in this problem, for the phase change at 100 °C and 1 atm	6
$\Delta S_{\text{vaporizn}} = (1.76 - 0.31) \text{ cal K}^{-1} \text{ g}^{-1}$	Given $(S_T - S^\ominus_{298}) = 0.31 \text{ cal K}^{-1} \text{ g}^{-1}$ for water at 100 °C and 1 atm Given $(S_T - S^\ominus_{298}) = 1.76 \text{ cal K}^{-1} \text{ g}^{-1}$ for steam at 100 °C and 1 atm	7
$= \Delta H_{\text{vaporizn}} / 373.1 \text{ K}$	From Eq 6	8
(a) $\Delta H_{\text{vaporizn}} = 373.1(1.76 - 0.31)$ $= 541 \text{ cal g}^{-1}$ Answer	Evaluating	9

(b) $\Delta H_{\text{vaporizn}} =$ $\{(H_T - H^{\ominus}_{298})_{\text{steam}} - (H_T - H^{\ominus}_{298})_{\text{water}}\}$ at 100 °C and 1 atm 541 cal g^{-1} $= 640 \text{ cal g}^{-1} - (H_T - H^{\ominus}_{298})_{\text{water}}$ $(H_T - H^{\ominus}_{298})_{\text{water}} = 99 \text{ cal g}^{-1}$	Using Eq 9 and given	10
(c) $G = H - TS$	Definition	11
$\Delta G = \Delta H - T\Delta S$	At constant T	12
$(G_T - G^{\ominus}_{298})_{\text{water}} = (H_T - H^{\ominus}_{298})_{\text{water}}$ $- 373.1 \bullet (S_T - S^{\ominus}_{298})_{\text{water}}$ $= 99 - 373.1 \bullet 0.31 = -16.7 \text{ cal g}^{-1}$ Answer	Substituting values	13
$(G_T - G^{\ominus}_{298})_{\text{steam}} = (H_T - H^{\ominus}_{298})_{\text{steam}}$ $- 373.1 \bullet (S_T - S^{\ominus}_{298})_{\text{steam}}$ $= 640 - 373.1 \bullet 1.76 = -16.7 \text{ cal g}^{-1}$ Answer	The two are equal as expected	

10. $\text{C}(\text{graphite}) \rightarrow \text{C}(\text{diamond})$ (298 K, 1 atm)

Equation	Basis for the equation	Eq. #
$\text{C}_{(\text{diamond})} + \text{O}_2 \rightarrow \text{CO}_2$ (298 K, 1 atm) $\Delta H = 94.484 \text{ kcal mol}^{-1}$ $\text{C}_{(\text{graphite})} + \text{O}_2 \rightarrow \text{CO}_2$ (298 K, 1 atm) $\Delta H = 94.030 \text{ kcal mol}^{-1}$ $\text{C}_{(\text{graphite})} \rightarrow \text{C}_{(\text{diamond})}$ (298 K, 1 atm) $\Delta H = 94.484 - 94.030 = 0.454$ kcal mol^{-1}	H is a state function	1
$\Delta S = S_{\text{diamond}} - S_{\text{graphite}}$ $= 0.5829 - 1.3609$ $= -0.7780 \text{ cal K}^{-1} \text{ mol}^{-1}$	Use given data at 298 K, 1 atm	2
$G = H - TS$	Definition	3
$\Delta G = \Delta H - T\Delta S$	At constant T	4
$\Delta G = 454 - 298 \bullet (-0.7780)$ $= 685.8 \text{ cal mol}^{-1}$ (298 K, 1 atm) Answer		5
$G^{\ominus}_{298}(\text{diamond}) - G^{\ominus}_{298}(\text{graphite}) =$ $685.8 \text{ cal mol}^{-1}$	$\ominus$ means 1 atm	6
$dG = Vdp - SdT$	One of the four fundamental equations of thermodynamics	7
$G(T) = G^{\ominus}_T + \int_1^p V dp$	For any pure material at a given temperature (dT=0)	8

$G_{298}(\text{diamond}) = G^{\ominus}_{298}(\text{diamond}) + \int_1^p V_{\text{diamond}} dp$ $G_{298}(\text{graphite}) = G^{\ominus}_{298}(\text{graphite}) + \int_1^p V_{\text{graphite}} dp$	Applying Eq 7 to each pure material	9
$C_{(\text{graphite})} \rightleftharpoons C_{(\text{diamond})} \text{ (298 K, p atm)}$ $G_{298}(\text{diamond, p}) - G_{298}(\text{graphite, p}) = 0$	At equilibrium at this value of p means G of graphite and G of diamond are equal at this p and 298 K.	10
$0 = 685.8 \text{ cal mol}^{-1} + \int_1^p V_{\text{diamond}} dp - \int_1^p V_{\text{graphite}} dp$	Using Eq 6, 9 and 10	11
$0 = 685.8 \text{ cal mol}^{-1} + (1.987/0.08206) \bullet (12 \text{ g}/3.513 \times 10^3 \text{ g L}^{-1})(p-1) - (12 \text{ g}/2.260 \times 10^3 \text{ g L}^{-1})(p-1)$	Using given densities, independent of pressure and 1 mol C = 12 g and $10^3 \text{ cm}^3 = 1 \text{ L}$ and use conversion 1.98722 cal = 0.0820578 L atm	12
$0 = 685.8 - 0.04586(p-1)$ $p-1 = 14950 \text{ atm} \quad \text{Answer for}$ $C_{(\text{graphite})} \rightleftharpoons C_{(\text{diamond})} \text{ (298 K, p atm)}$	Solving for p	
$C_{(\text{graphite})} \rightleftharpoons C_{(\text{diamond})} (1273 \text{ K, p atm})$ $G_{1273}(\text{diamond, p}) - G_{1273}(\text{graphite, p}) = 0$ $0 = G^{\ominus}_{1273}(\text{diamond}) - G^{\ominus}_{1273}(\text{graphite}) + \int_1^p V_{\text{diamond}} dp - \int_1^p V_{\text{graphite}} dp$ Solve for p	To do the same calculation for 1000°C. We need the value $G^{\ominus}_{1273}(\text{diamond}) - G^{\ominus}_{1273}(\text{graphite})$, for which we need molar entropies S at 1000°C, 1 atm, and also ΔH at 1000°C, 1 atm. S_{1273} for graphite = $1.3609 \text{ cal K}^{-1} \text{ mol}^{-1} + \int_{298}^{1273} (C_{p, \text{graphite}}/T) dT$ S_{1273} for diamond = $0.5829 \text{ cal K}^{-1} \text{ mol}^{-1} + \int_{298}^{1273} (C_{p, \text{diamond}}/T) dT$ $\Delta H_{1273}(\text{graphite}) = \Delta H_{298} + \int_{298}^{1273} C_{p, \text{graphite}} dT$ $\Delta H_{1273}(\text{diamond}) = \Delta H_{298} + \int_{298}^{1273} C_{p, \text{diamond}} dT$ To estimate these quantities, we need to find C_p data for the two forms over the range 298 to 1273K.	