

$$1 \text{ J} = 1 \text{ kg m}^2 \text{ s}^{-2} \quad k_B = 1.38066 \times 10^{-23} \text{ J K}^{-1}$$

$$R = N_{\text{Avogadro}} k_B$$

$$R = 8.31441 \text{ J mol}^{-1} \text{ K}^{-1} = 1.98718 \text{ cal mol}^{-1} \text{ K}^{-1} = 0.082057 \text{ L atm mol}^{-1} \text{ K}^{-1}$$

$$p/p_0 = \exp[-(M/RT)gz] \quad \text{barometric formula}$$

$$C_p - C_v = \{p + (\partial U/\partial V)_T\}(\partial V/\partial T)_p \quad (\partial H/\partial p)_T = [p + (\partial U/\partial V)_T](\partial V/\partial p)_T + V$$

$$\mu_{JT} = (\partial T/\partial p)_H \quad (\partial H/\partial p)_T = -C_p \mu_{JT}$$

$$\text{monatomic gas molar heat capacity: } C_v = (3/2)R$$

1. Investigate some of the technicalities of ballooning using the perfect gas law.

Suppose your balloon has a capacity of 10^3 m^3 is filled with He at 20°C and 1 atm pressure. Assume that the volume of the balloon is constant, the atmosphere isothermal at 20°C and the molecular weight of air is 28.8 and the ground level pressure is 1 atm. The balloon itself is made of material whose mass may be neglected compared to the load.

(a) What is the density of air at ground level? *use ideal gas law*

$$\rho_{\text{air}} = \left(\frac{P}{RT}\right)M = \frac{1 \text{ atm } 28.8 \text{ g mol}^{-1}}{0.082057 \text{ L atm mol}^{-1} \text{ K}^{-1} 293 \text{ K}} = 1.197 \text{ g/L}$$

(b) What is the load that the balloon can lift at ground level? [Hint: Archimedes]

The balloon can lift a load because the He balloon displaces an equal volume of air, but itself has a much smaller mass.

$$m_{\text{He}} + m_{\text{Load}} = m_{\text{displaced air}}$$

$$\therefore m_{\text{Load}} = V(\rho_{\text{air}} - \rho_{\text{He}}). \quad \text{At ground level } p = 1 \text{ atm,}$$

$$\rho_{\text{He}} = \left(\frac{P}{RT}\right)M = \frac{(1)(4)}{(0.082057)(293)} = 0.166 \text{ g/L}$$

$$\therefore m_{\text{Load}} = 10^3 \text{ m}^3 \left(\frac{1000 \text{ cm}^3}{1 \text{ m}^3}\right) \left(\frac{1 \text{ L}}{10^3 \text{ cm}^3}\right) (1.197 - 0.166) = 10^3 \text{ L } (1.197 - 0.166) \text{ g/L} = 1.031 \times 10^3 \text{ g}$$

(c) If the balloon is loaded with 80% of the load that it can lift at ground level, at what height will the balloon come to rest?

$$m_{\text{He}} + m_{\text{Load}} = m_{\text{displaced air}}$$

$$10^3 (0.166) + 0.80 (1.031 \times 10^3) = 10^3 (1.197 p/p_0)$$

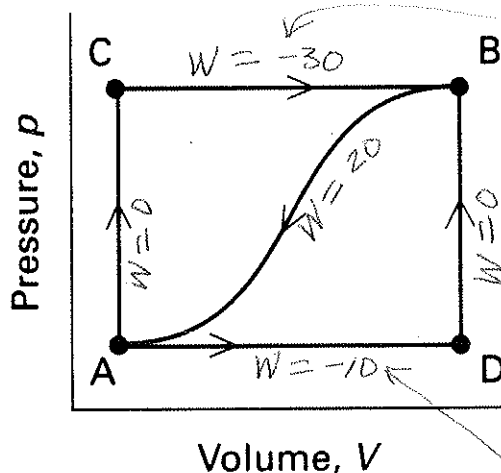
$$\therefore p/p_0 = 0.8277 = e^{-Mgz/RT}$$

$$\ln 0.8277 = -1.1586 \times 10^{-4} = -\frac{Mgz}{RT} = \frac{-28.8 \times 10^{-3} \text{ kg mol}^{-1} 9.8 \text{ m s}^{-2} Z (\text{meters})}{8.3144 \text{ J mol}^{-1} \text{ K}^{-1} 293 \text{ K}}$$

$$\therefore Z = 1.632 \times 10^3 \text{ meters}$$

[Note: if we could neglect the mass of the He, then the answer is very simple: $0.80 = p/p_0$]

2. When a system is taken from state A to state B along the path ACB in the figure below, 80 J of heat flows into the system and the system does 30 J of work.



Use
First Law
in each
case

(a) How much heat flows into the system along path ADB if the work done is 10 J?

Given $q_{ACB} = 80$ and $W_{ACB} = -30$
 $\therefore U_B - U_A = q_{ACB} + W_{ACB} = 80 - 30 = 50 = q_{ADB} + W_{ADB}$ (since U is a state function)
 $= q_{ADB} - 10$
 $\therefore q_{ADB} = 60 \text{ J}$ ($= q_{AD} + q_{DB}$, of course)

(b) When the system is returned from state B to A along the curved path, the work done on the system is 20 J. Does the system absorb or liberate heat, and how much?

From (a) $U_A - U_B = -50 = q_{BA} + W_{BA} = q_{BA} + 20$
 $\therefore q_{BA} = -70 \text{ J}$ (since U is a state function)

The system liberates heat to the surroundings

(c) If $U_D - U_A = +40 \text{ J}$, find the heat absorbed in each of the processes AD and DB.

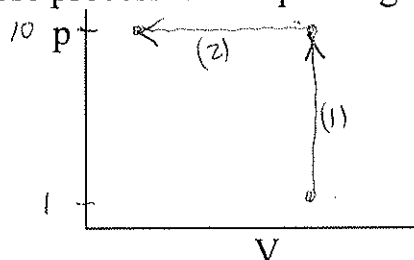
(Given) $U_D - U_A = +40 = q_{AD} + W_{AD}$ But $W_{AD} = -10$ since $W_{ADB} = -10$ and $W_{DB} = 0$
 $\therefore q_{AD} = +50 \text{ J}$
 Also from (a), $q_{AD} + q_{DB} = 60 \text{ J} \therefore q_{DB} = 10 \text{ J}$

$$\therefore C_p - C_v = R$$

3. Assume that air behaves as an ideal gas with $C_p = (7/2)R$.

$$C_v = \frac{5}{2}R$$

(a) In one experiment 1.00 mole of "air molecules" is compressed from 1.00 atm to 10.0 atm at 25°C by the following reversible process: (1) heating at constant volume to the final pressure, followed by (2) cooling at constant pressure to 25°C. Sketch these processes on a pV diagram.



(Initial)₁

(Final)₁ & (Initial)₂

(Final)₂

$$P_1 = 1 \text{ atm}$$

$$P = 10 \text{ atm}$$

$$P = 10 \text{ atm}$$

$$T = 298 \text{ K}$$

$$T = ? = 10 \frac{R \cdot 298}{R} = 2980 \text{ K}$$

$$T = 298 \text{ K}$$

$$V = \frac{R \cdot 298}{1} = 24.45$$

$$V = \frac{R \cdot 298}{1} = 24.45$$

$$V = \frac{R \cdot 298}{10} = 2.445$$

Calculate ΔU , ΔH , q , and W , in kJ for each step in the process and for the overall process.

step 1 constant vol.	step 2 constant p	overall sum step 1 + 2
$q = q_v = \int_{298}^{2980} C_v dT$ $= \frac{5}{2} 8.314 [2980 - 298]$ $= 55.748 \text{ kJ}$	$q = q_p = \int_{298}^{2980} C_p dT$ $= \frac{7}{2} 8.314 [2980 - 298]$ $= -78.047 \text{ kJ}$	$q = 55.748 - 78.047$ $= -22.3 \text{ kJ}$
$W = \int p_{\text{ext}} dV$, $dV = 0$ $\therefore W = 0$	W get from $W = \Delta U - q$ $= -55.748$ $- -78.047$ $= +22.3 \text{ kJ}$	$W = 0 + 22.3 \text{ kJ}$ $= 22.3 \text{ kJ}$
ΔU $dU = C_v dT + \left(\frac{\partial U}{\partial V}\right)_T dV$ $\Delta U = q_v = 55.748 \text{ kJ}$	ΔU $dU = C_v dT + 0$ $\Delta U = \frac{5}{2} 8.314 [2980 - 298]$ $= -55.748 \text{ kJ}$	$\Delta U = 0$ since back to same temperature (298 K) and ideal
ΔH $dH = C_p dT + \left(\frac{\partial H}{\partial p}\right)_T dp$ $\Delta H = \frac{7}{2} 8.314 [2980 - 298]$ $= 78.047 \text{ kJ}$	ΔH $dH = C_p dT + \left(\frac{\partial H}{\partial p}\right)_T dp$ $\Delta H = \frac{7}{2} 8.314 [2980 - 298]$ $= -78.047 \text{ kJ}$	$\Delta H = 0$ since ... (same as above)

4. n moles of a gas obeying the equation of state $p(V-nb) = nRT$ ($b = 10^{-1} \text{ L mol}^{-1}$) and has $(\partial U/\partial V)_T = 0$, $(\partial H/\partial p)_T = -b$ is subjected to an isothermal reversible expansion from an initial volume of 1.00 L to 24.8 L at 298 K. Calculate the values of ΔU , ΔH , q , and W , in kJ (in terms of n).

q get from $q = \Delta U - W$ $= -W$	W reversible $P_{op} = P_{gas}$ $W = \int dW = - \int P_{op} dV = -nR 298 \int_{1.0L}^{24.8L} \frac{dV}{V-nb}$ $W = -nR 298 \ln \left(\frac{24.8 - 0.1n}{1.0 - 0.1n} \right)$
ΔU $dU = C_v dT + \underbrace{\left(\frac{\partial U}{\partial V} \right)_T}_{\text{zero given}} dV$ $dT = 0$ $\therefore \Delta U = 0$	ΔH $dH = C_p dT + \underbrace{\left(\frac{\partial H}{\partial p} \right)_T}_{-b \text{ given}} dp$ $dT = 0$ $\Delta H = \int \left(\frac{\partial H}{\partial p} \right)_T dp = -b \int_{p= \frac{nR 298}{24.8 - 0.1n}}^{p= \frac{nR 298}{1.0 - 0.1n}} dp$ $= -b nR 298 \left[\frac{1}{24.8 - 0.1n} - \frac{1}{1.0 - 0.1n} \right]$

5. Calculate the standard enthalpy of formation $\Delta_f H^\ominus$ of KClO_3 from the enthalpy of formation of KCl ($-436.75 \text{ kJ mol}^{-1}$) together with the following information all at 298 K:



$$-89.4 \text{ kJ mol}^{-1} = 2 \times (-436.75) + 3 \times 0 - 2 \Delta_f H^\ominus_{\text{KClO}_3}$$

$$\Delta_f H^\ominus_{\text{KClO}_3} = \frac{2(-436.75) + 89.4}{2} = -392.05 \text{ kJ mol}^{-1}$$

6. A cylindrical container of fixed total volume is divided into three sections, S_1 , S_2 , and S_3 . The sections S_1 and S_2 are separated by an adiabatic piston, whereas S_2 and S_3 are separated by a diathermic (heat conducting) piston. The pistons can slide along the walls of the cylinder without friction. Each section of the cylinder contains 1.00 mole of a perfect diatomic gas [$C_V = (5/2)R$]. Initially the gas pressure in all three sections is 1.00 atm and the temperature is 298 K. The gas in S_1 is heated slowly until the temperature of the gas in S_3 reaches 348 K.

see next page

Find the final temperature, pressure, and volume, as well as the change in internal energy for each section.

S_1	S_2	S_3
p_f	p_f	p_f
V_f	V_f	V_f
T_f	T_f	T_f
ΔU	ΔU	ΔU

Determine the total energy supplied to the gas in S_1 .

S ₁	S ₂	S ₃
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Initial: $p_1 = 1 \text{ atm}$ $p_2 = 1 \text{ atm}$ $p_3 = 1 \text{ atm}$
 $T_1 = 298 \text{ K}$ $T_2 = 298 \text{ K}$ $T_3 = 298 \text{ K}$
 ideal: $V_1 = ? = 298R/1 = 24.4 \text{ L}$ $V_2 = ? = 298R/1 = 24.4 \text{ L}$ $V_3 = ? = 298R/1 = 24.4 \text{ L}$

Since fixed total volume, total work = 0, $W_1 + W_2 + W_3 = 0$

Since adiabatic piston between S₁ and S₂, $q_2 + q_3 = 0$

Since pistons are free to slide, then final $p_{f1} = p_{f2} = p_{f3} = p_f$

Since diathermic piston between S₂ and S₃, then T_{f2} is same as $T_{f3} = 348 \text{ K}$

Since S₂ and S₃ are at same final p_f and T_f then $V_{f2} = V_{f3}$

What can we calculate?

$dU = C_V dT + (\partial U / \partial V)_T dV$ but $(\partial U / \partial V)_T = 0$ for an ideal gas. Therefore,

$$\Delta U_2 = C_V [348 - 298] = (5/2)R[348 - 298] = 250 \text{ cal}$$

$$\Delta U_3 = C_V [348 - 298] = (5/2)R[348 - 298] = 250 \text{ cal}$$

First law: $\Delta U_2 = q_2 + W_2$ and $\Delta U_3 = q_3 + W_3$

But since $q_2 + q_3 = 0$ and $W_1 + W_2 + W_3 = 0$, then

$$W_1 = -(W_2 + W_3) = -(\Delta U_2 + \Delta U_3) = -(250 + 250) = -500 \text{ cal}$$

Ideal gases in S₂ and S₃ together went through an adiabatic reversible (infinitely slowly) compression brought about by expansion of S₁.

Therefore, $\ln\{ [T_{f2}/T_2]^{C_V/R} \} = \ln [V_2/V_{f2}]$ holds.

$$\ln\{ [348/298]^{5/2} \} = \ln [298R/V_{f2}] , \text{ solve for } V_{f2} = 16.59 \text{ L} = V_{f3}$$

Now ideal gas equation gives p_f from T_{f2} and V_{f2} : $p_f = R(348)/V_{f2} = 1.72 \text{ atm}$

Now we know also that fixed total volume is the same as total initial volume,

$$V_{f1} + 2V_{f2} = 3 \cdot R \cdot 298 / 1 , \text{ solve for } V_{f1} , V_{f1} = 40.16 \text{ L}$$

In S₁ we know p_f and V_{f1} , apply ideal gas law: $p_f V_{f1} = R(T_{f1})$, solve for T_{f1}

$$T_{f1} = 1.72 \text{ atm}(40.16 \text{ L}) / 0.082057 = 841.8 \text{ K}$$

In S₁ can now apply First Law: $\Delta U_1 = C_V [T_{f1} - 298] = \dots = q_1 + W_1$, solve for q_1
 $(5/2)R[841.8 - 298] = 2701.6 \text{ cal} = q_1 - 500 \text{ cal}$, $q_1 = 3202 \text{ cal}$ which is the
 total energy supplied to the gas in S₁.

S ₁	S ₂	S ₃
p_f 1.72 atm	p_f 1.72 atm	p_f 1.72 atm
V_f 40.16 L	V_f 16.59 L	V_f 16.59 L
T_f 841.8 K	T_f 348 K	T_f 348 K
ΔU 2701.6 cal	ΔU 250 cal	ΔU 250 cal

The total energy supplied to the gas in S₁ = 3202 cal